



Sustainable Lignocellulosic Biofuels Co-production and Agro-industrial Wastes Treatment using a Multi-feed Biorefinery

Western Mexico Case Study

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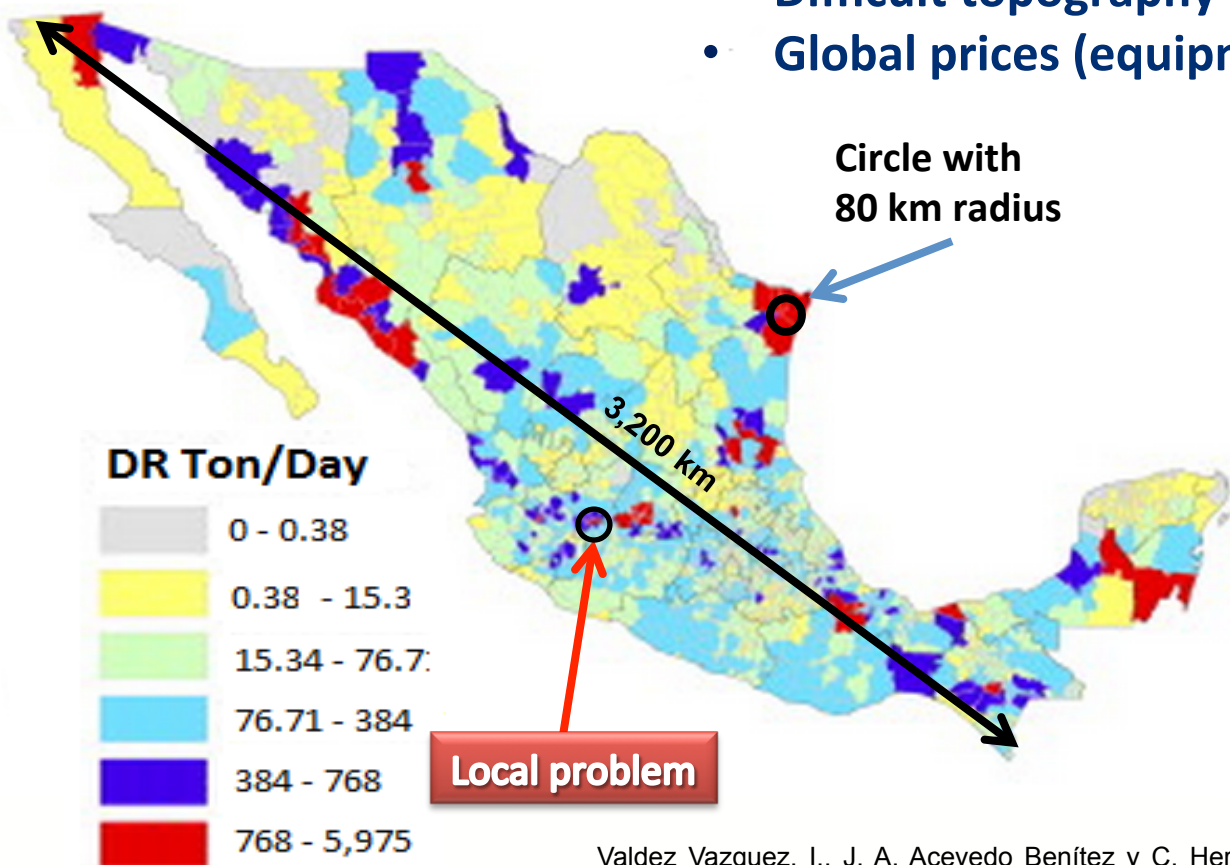


Motivation

- Biorefineries for the Mexican context
- Biorefinery design
 - Biofuels **co-production** (bioethanol, biohydrogen and biogas)
 - **Electricity**-steam cogeneration
 - **Multi-feed** with local agro-industrial residues and wastes
- Proposal of a biorefinery for bioenergy production designed with **sustainability criteria**, instead of techno-economic criteria only
- Solution for
 - **Restricted availability of biomass**
 - **Local environmental pollution**
- Affordable solution at local level

Availability of Agricultural Residues in Mexico

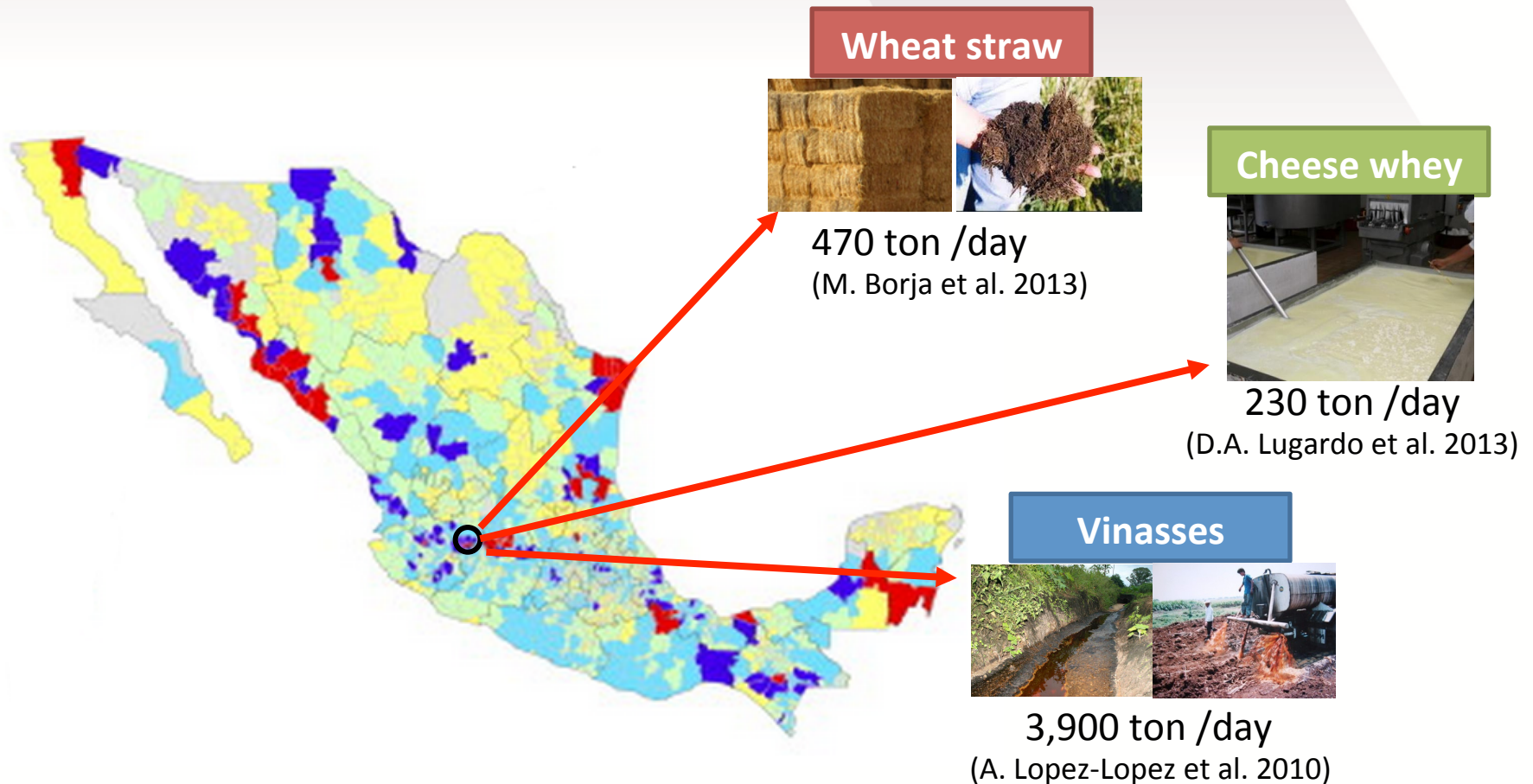
- Crop diversity
- “Large enough” amounts
- Scattered along vast territory
- Difficult topography → difficult collection
- Global prices (equipment, resources, logistics)



Crop	PCRI	Prod Mton/year	Res prod Mton/year
Wheat	1.5	3.4	5.1
Corn	1.5	21.9	32.9
Sorghum	1.5	5.5	8.2
Sugarcane	0.15	50.6	7.6
Coffee Cherry (pulp)	0.24	1.5	31.5
Agave (bagasse)	0.12	1.2	1.5

Local Problem in a Western Region in Mexico

- Wheat straw and composted wheat straw
- Wastes from tequila and dairy industries with high COD





Design Basis

- Economies and feedstock availability suitable for 500 ton/day
- Increasing biorefinery **sustainability** by
 - Reducing direct operation/capital cost
 - If biofuels production already efficient, alternative: improving process tasks not related to biofuels production
 - **Efficient process water usage**
 - CO₂ reutilization
 - Heat and **electricity** co-generation

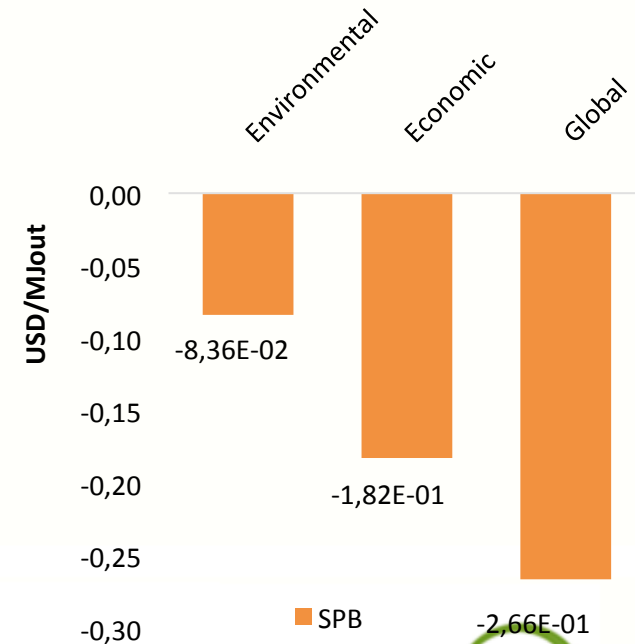
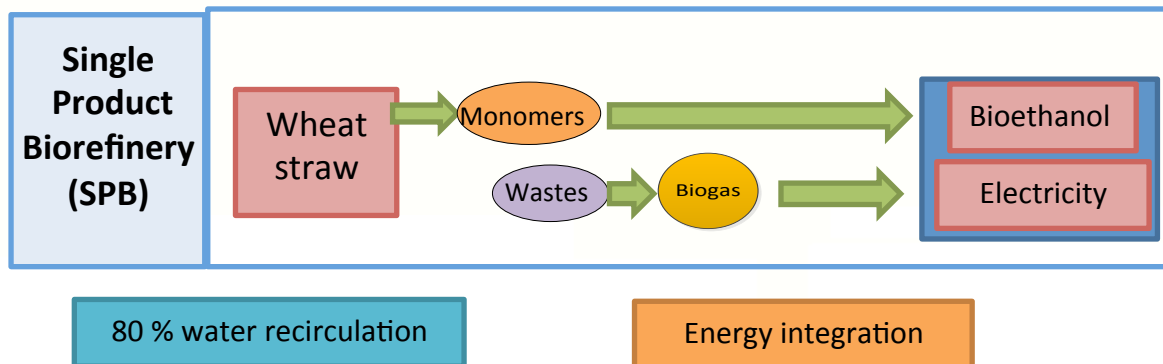
A. Sanchez, G. Magaña, D. Gomez, and M. Solis. (2014) Bidimensional sustainability analysis of lignocellulosic ethanol production processes. *Method and case study. Biofuels, Bioproducts and Biorefining*, 8:670–685.



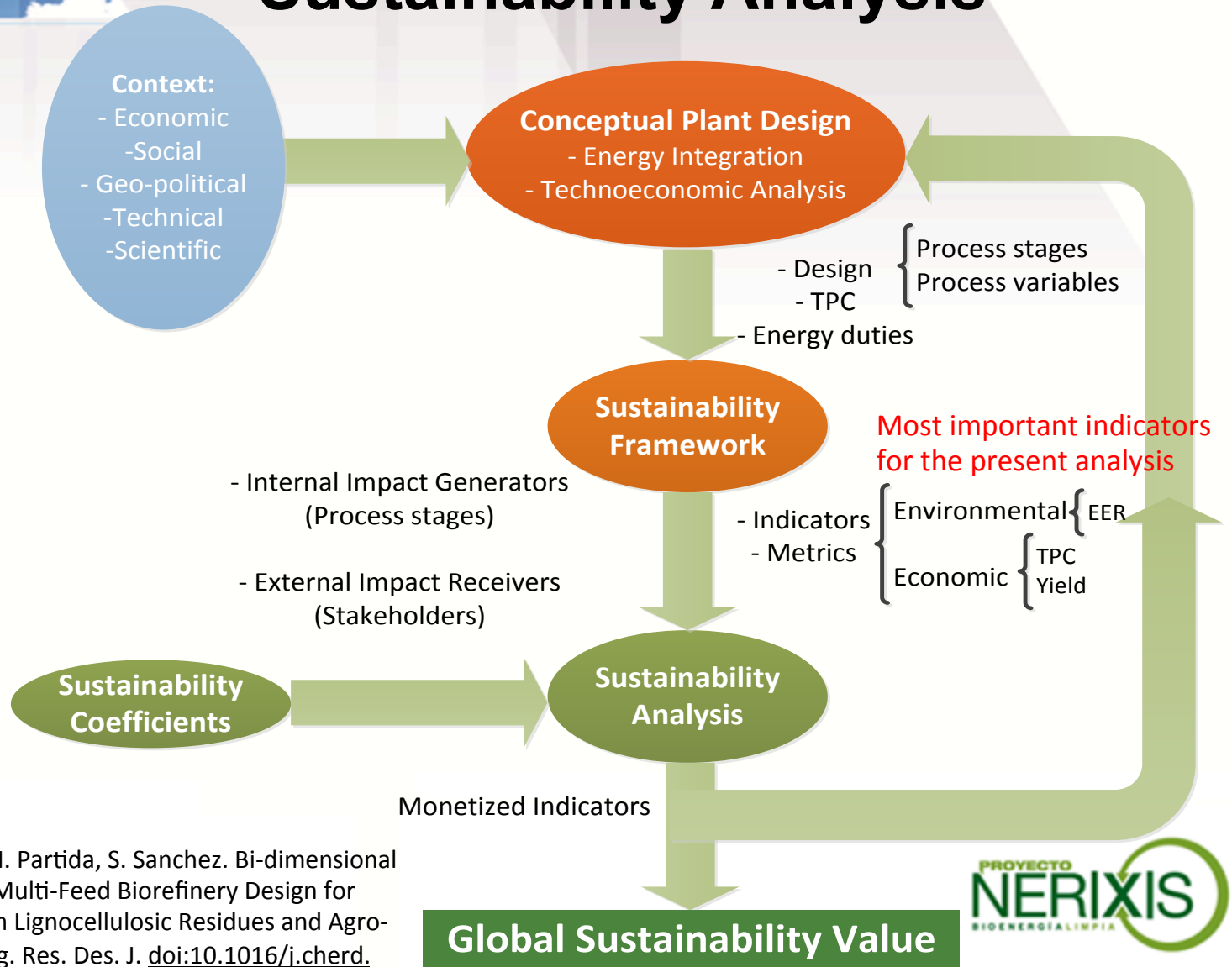
Design Strategy based on Bidimensional Sustainability Criteria

- Design a multi-feed biorefinery for 500 ton wheat straw (compost)/day dry basis
- Increasing electricity production: treatment of 50% whey and 10% vinasses available in the region
- Design MPB as sustainable as our most sustainable biorefinery design (SPB)

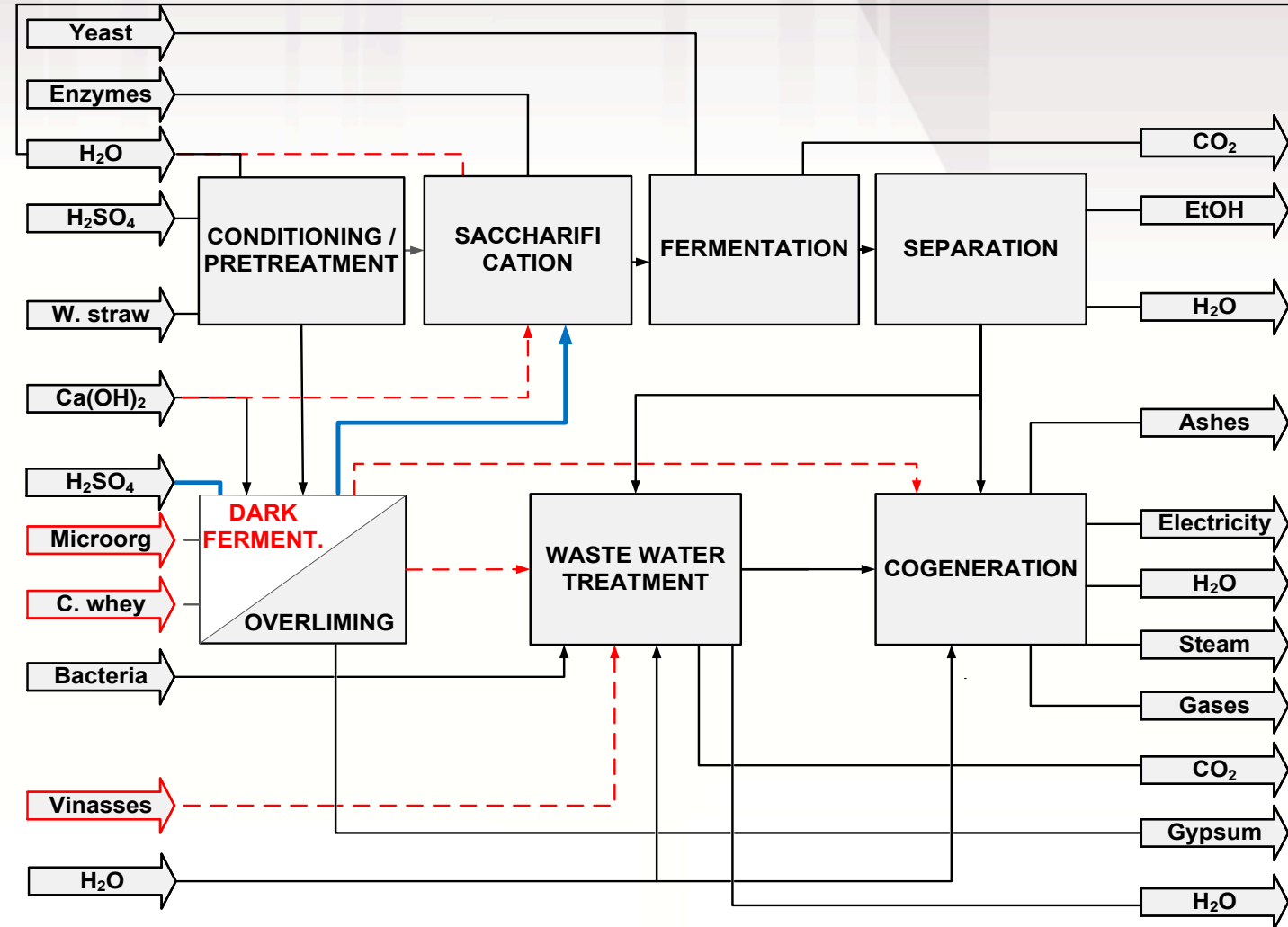
SPB Benchmark



Conceptual Design and Bidimensional Sustainability Analysis



Multi-feed Coproduction Scheme



Biorefinery
Complexity
Index

MPB10
BCI=38

SPB BCI= 29

BOTH DESIGNS →

MPB10 - - - - -

SPB ———





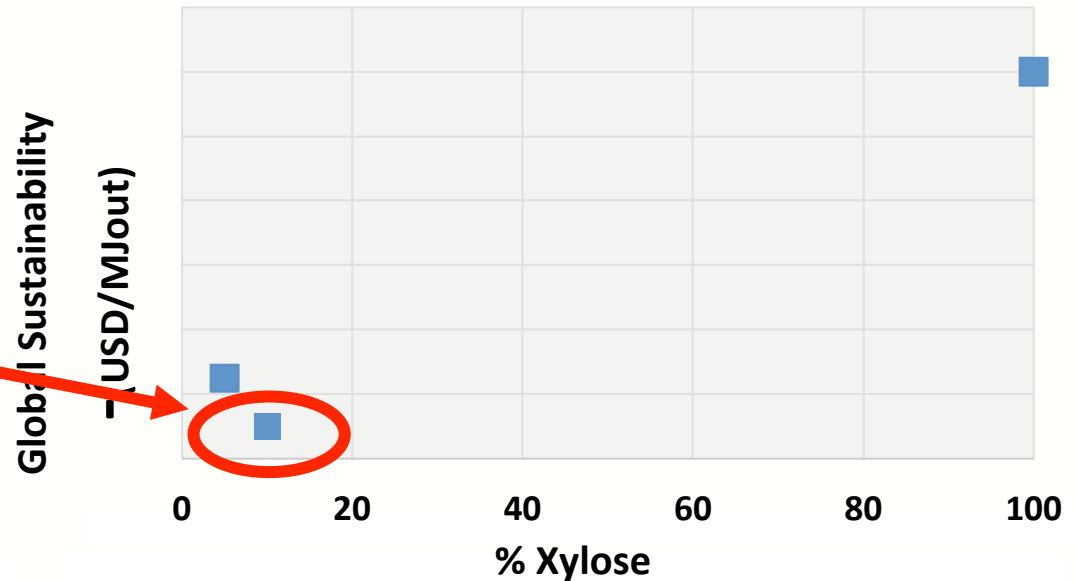
Design Strategy based on Bidimensional Sustainability Criteria

- Reducing xilose to alcoholic fermentation means
 - reducing bioethanol production
 - Increasing hydrogen/biogas production
- A.M. Lopez-Hidalgo et al. 2013: at least $0.07 \text{ kg}_{\text{xylose}}/\text{kg}_{\text{lactose}}$ for optimal hydrogen and organic acids production with *E. coli WHDL*. (60% higher than WSH alone @ 28°C)
- Design parameter: minimum xilose/whey ratio for improved H2 and biogas enhancers production in BF

10% of xylose from pretreatment for H₂ production

=

$0.3 \text{ kg}_{\text{xylose}}/\text{kg}_{\text{lactose}}$



A.M. Lopez-Hidalgo, Z.D. Alvarado-Cuevas, A. Sanchez, L.G. Ordonez-Acevedo, and A. De Leon-Rodriguez. (2013). Production of biohydrogen by fermentation using a mixture of cheese whey and wheat straw hydrolysate. In Proceedings of CIAB 2. Iberoamerican on Biorefineries Congress, Jaen, España.

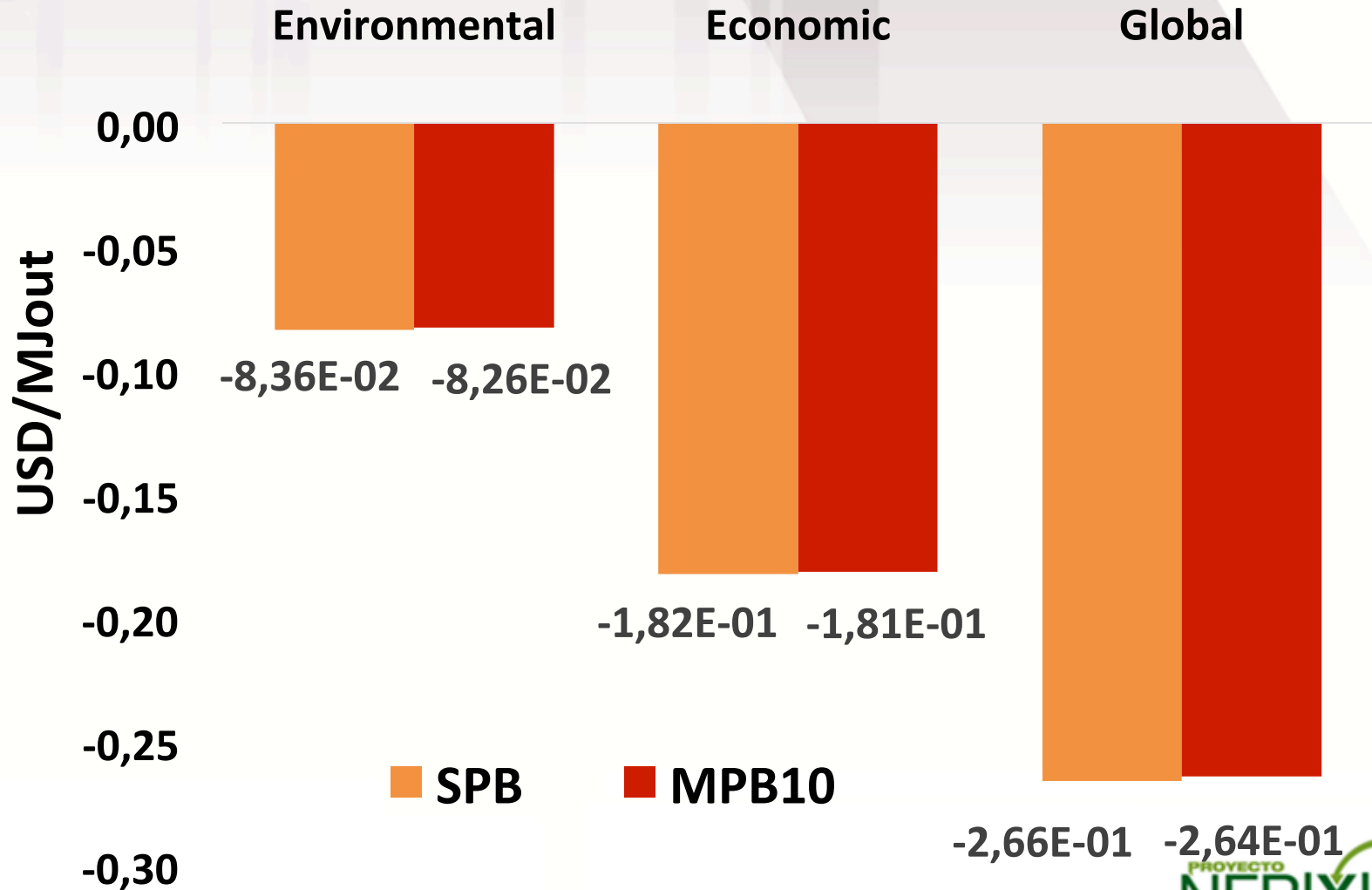


Results



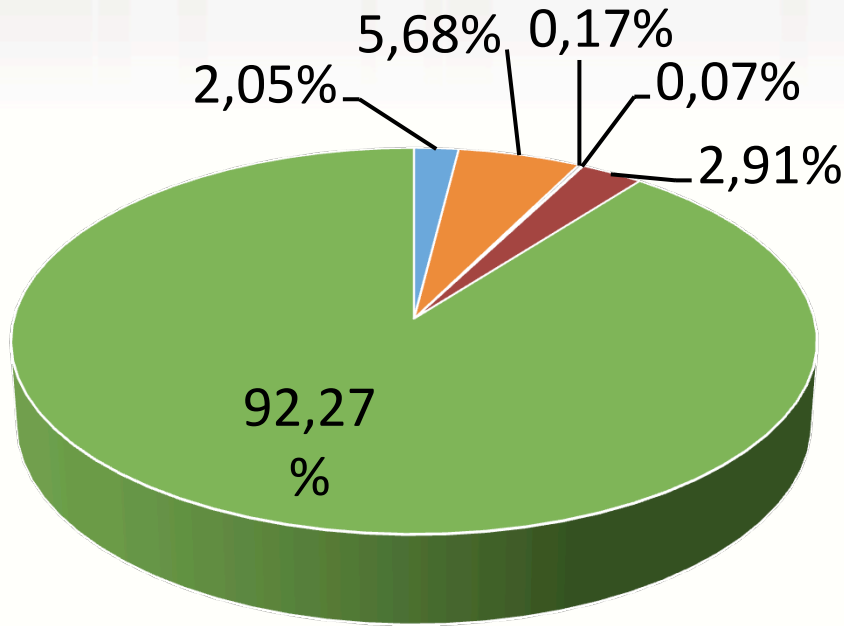


Global Sustainability Values

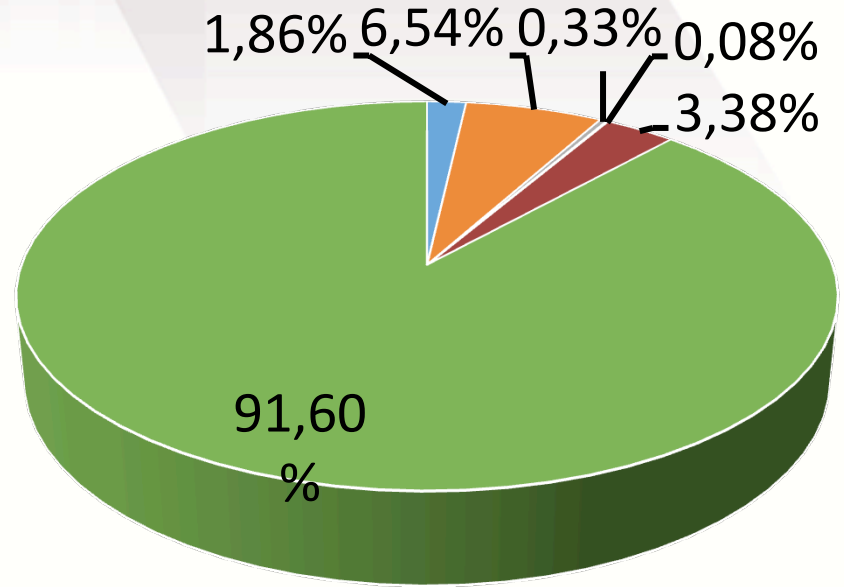




Environmental Indicators Contribution to Global Sustainability



MPB10

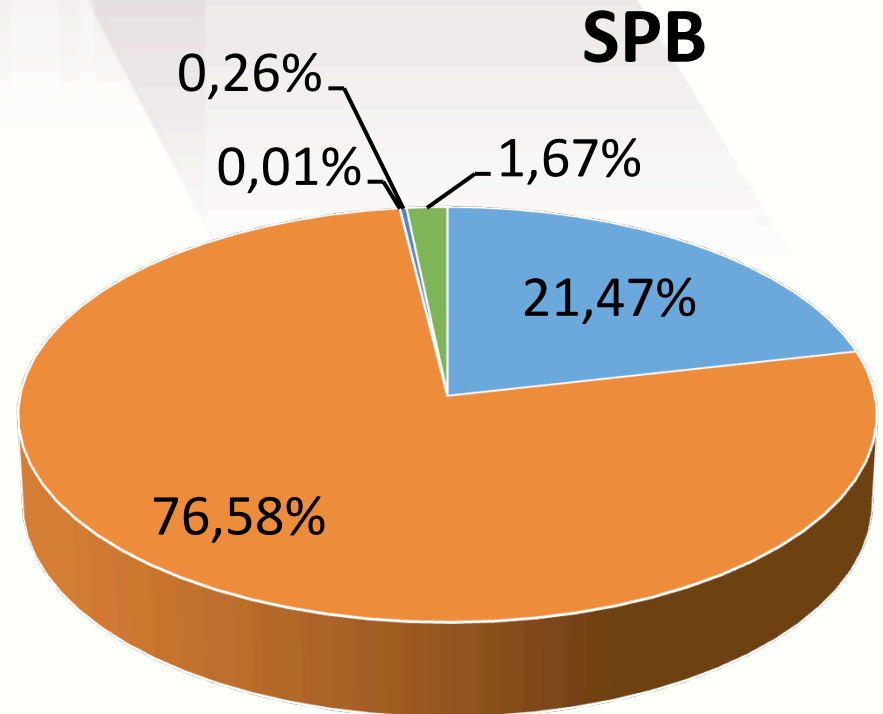
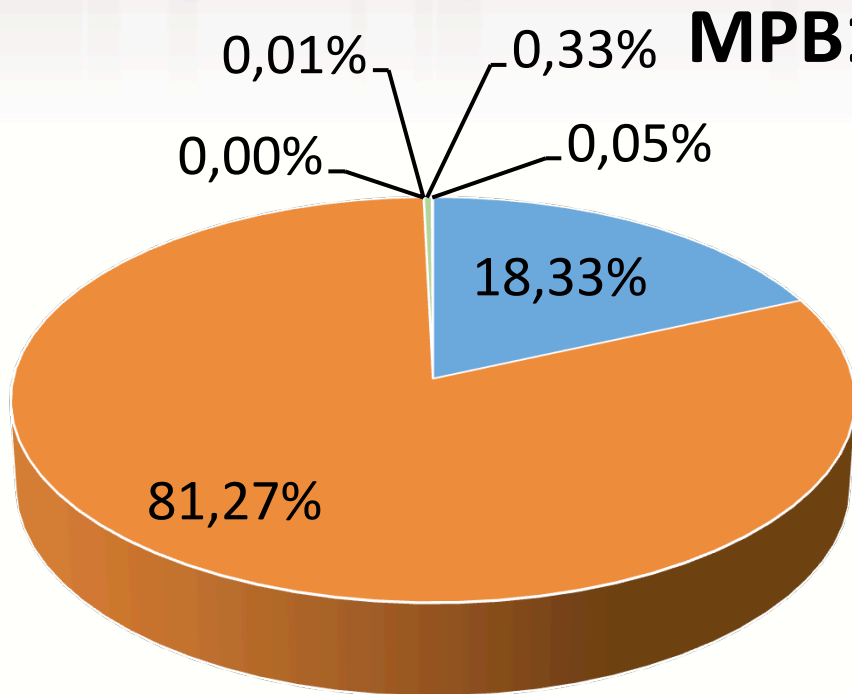


SPB

- Emitted GHG
- Emitted non GHG
- Water consumption
- Water quality
- Amount of produced solid wastes
- End use energy ratio (EER)



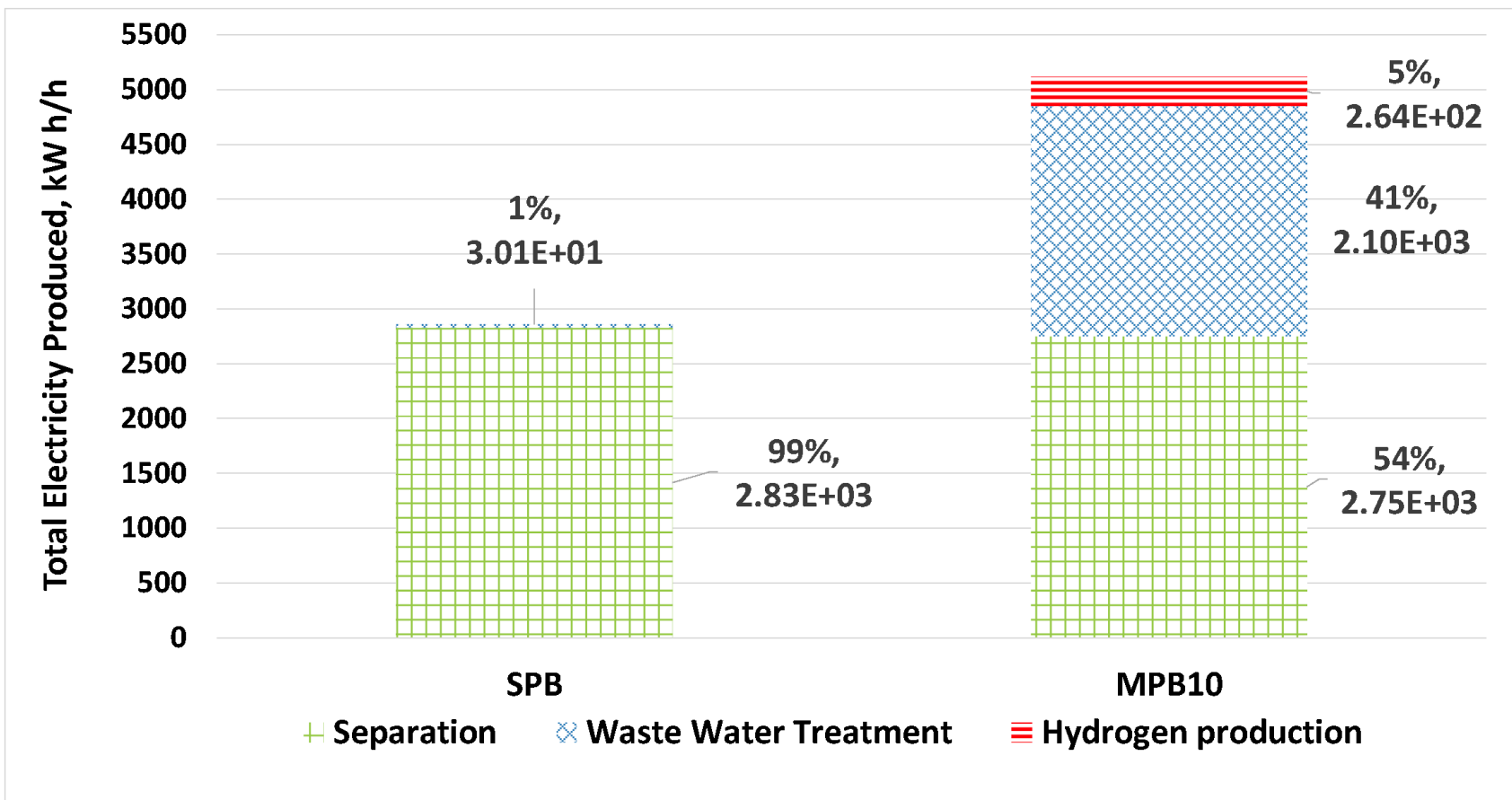
Economic Indicators Contribution to Global Sustainability



- Yield
- Production cost
- Reduction of fossil fuels imports
- Fraction of the energy demand (for transport) that the plant can cover
- Fraction of the total national bioenergy that is produced in the plant
- Plant's electrical productivity

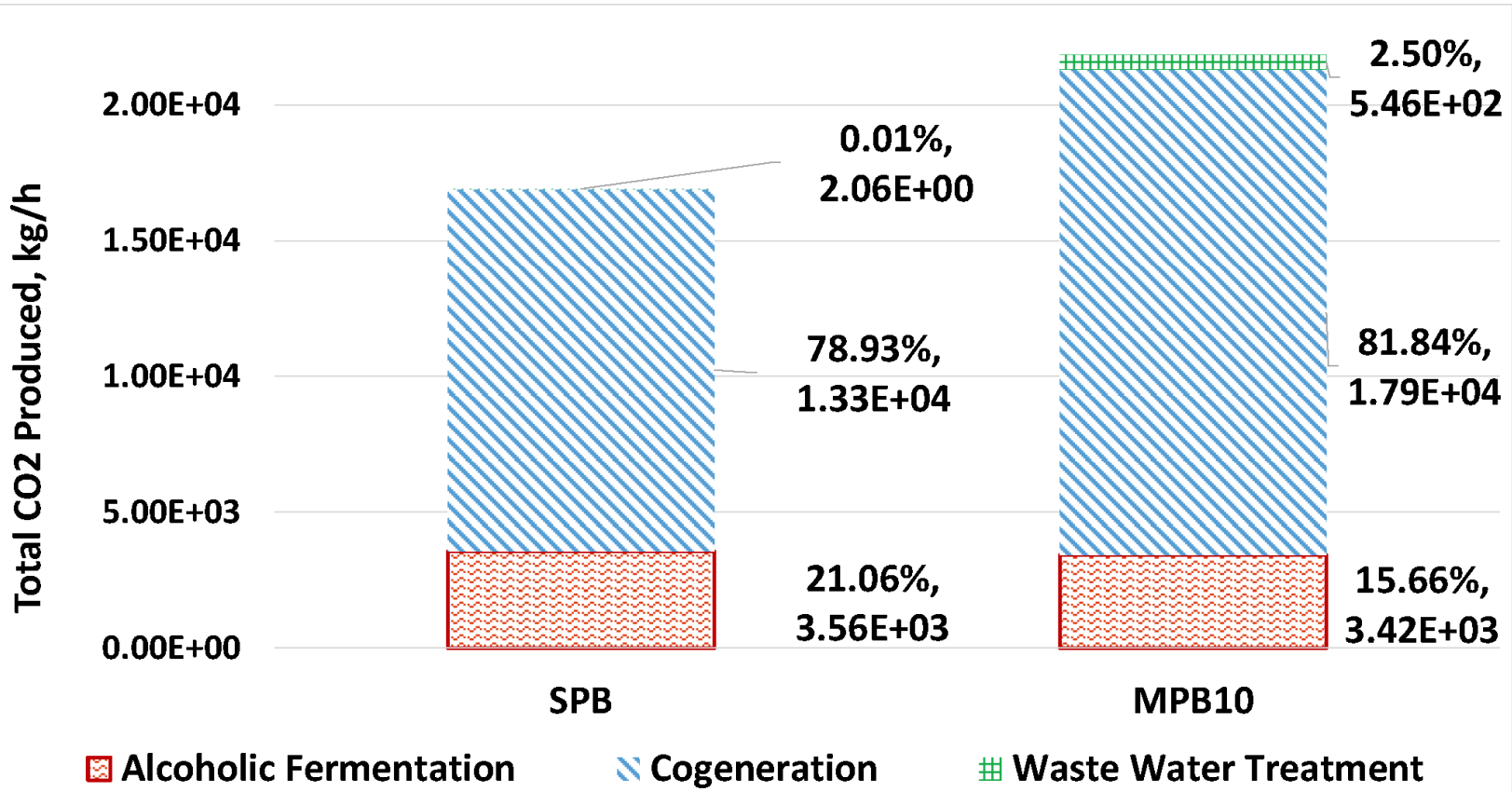


Process Stages Contribution to Electricity Generation





Process Stages Contribution to CO₂ Production





Conclusions





Conclusions

- Higher process complexity (MPB10 BCI=38 vs SPB BCI= 29)
- MPB10 with
 - Lower water consumption (50% lower)
 - Fewer solid wastes (15% lower)
 - Similar EER (6% higher)
 - Higher energy yield (18% higher)
 - Higher electricity productivity (40% higher)
 - Only 4% lower bioethanol production than SPB and the added benefit of solving a severe environmental pollution problem.
- **However**, SPB TPC per etOH (1.20 USD/L) and per energy unit (0.141 USD/MJ_{out}) produced are 30% and 5% smaller than MPB10 (1.56 USD/L, 0.148 USD/MJ_{out})
- **Nevertheless**
 - An alternative for limited biomass availability
 - An important environmental pollution problem is solved. Not accounted in the design criteria!
- Design criteria beyond techno-economic parameters?

THANK YOU

Acknowledgements



RED TEMÁTICA DE
BIOENERGÍA



Red Temática Mexicana para el
Aprovechamiento Integral Sustentable y
Biotecnología de los Agaves (AGARED)



CONACYT
Consejo Nacional de Ciencia y Tecnología

Project 247498

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