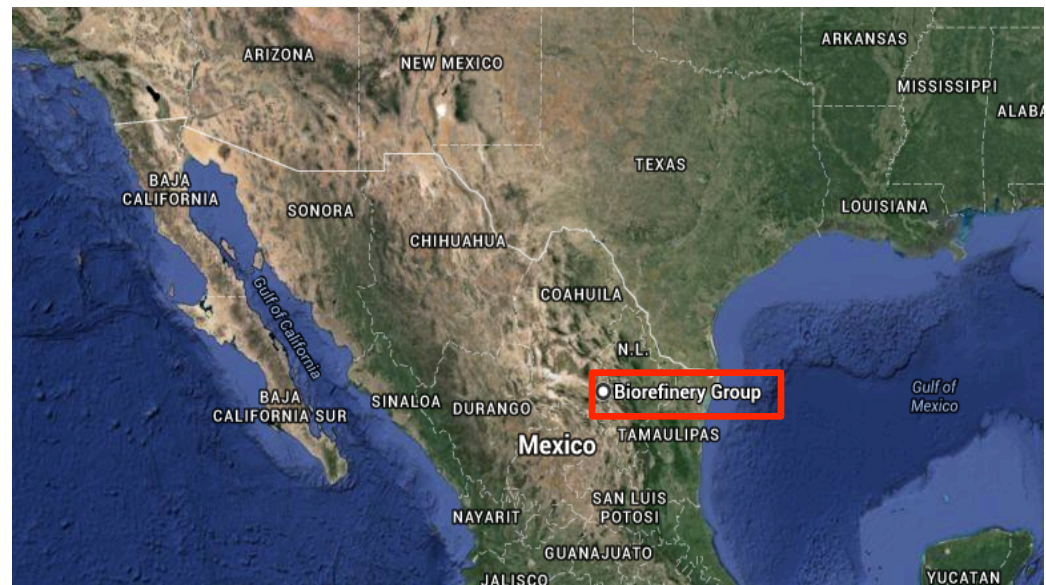
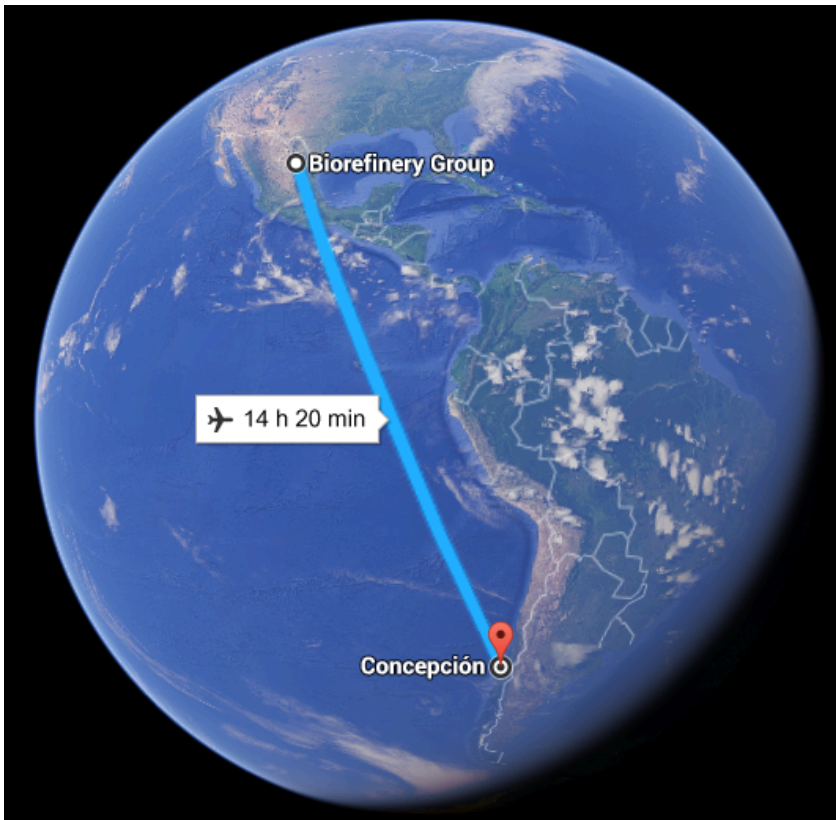




Comparison between microwave and conduction convection heating for autohydrolysis processing in the production of high added value compounds and substrates for biofuel under the biorefinery concept

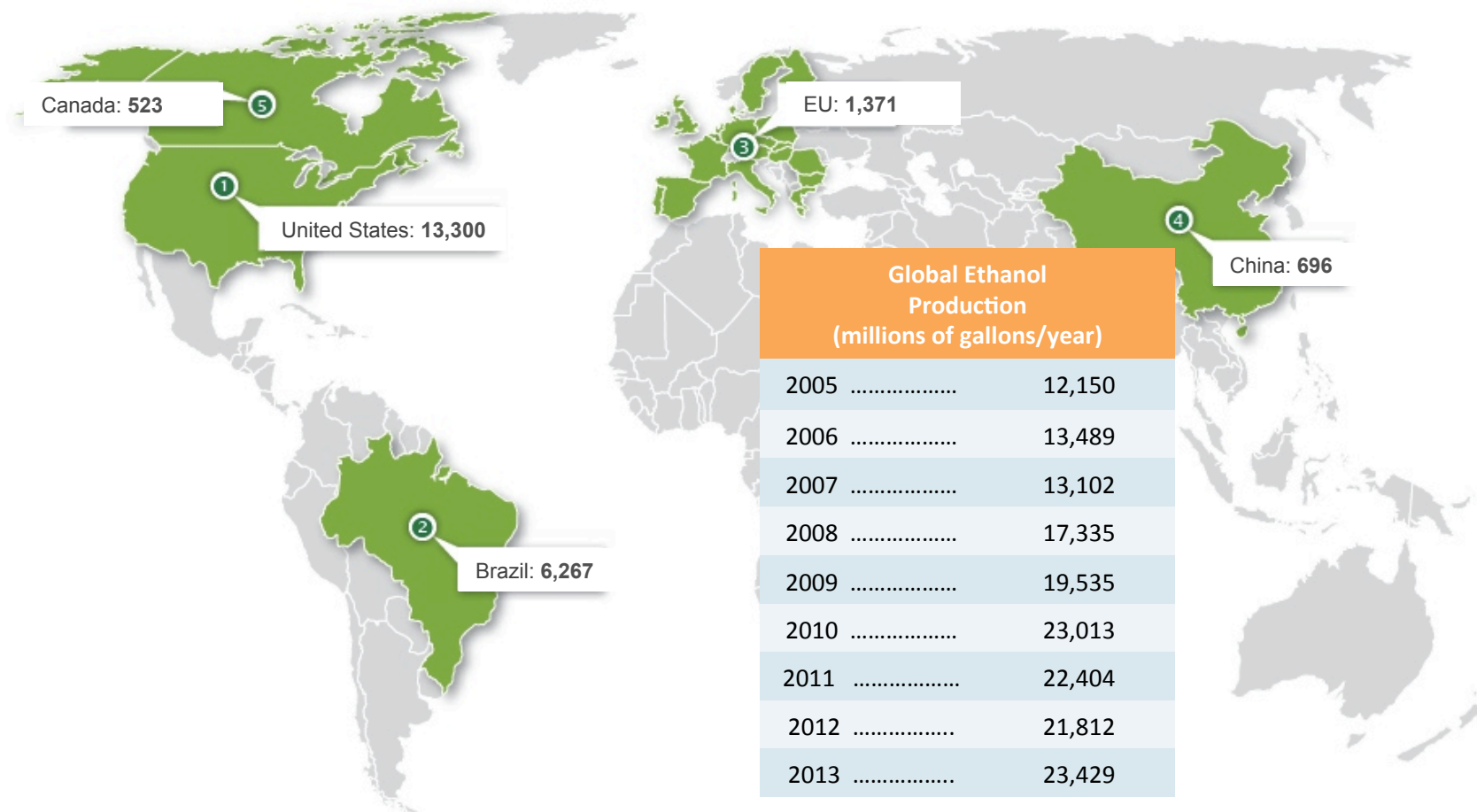
Anely A. Lara-Flores, Jesus Velazquez-Lucio, Elisa Zanuso, Rosa M. Rodríguez-Jasso, Cristóbal N. Aguilar, Héctor A. Ruiz

Biorefinery Group
Food Research Department, School of Chemistry
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Saltillo, Coahuila, Mexico

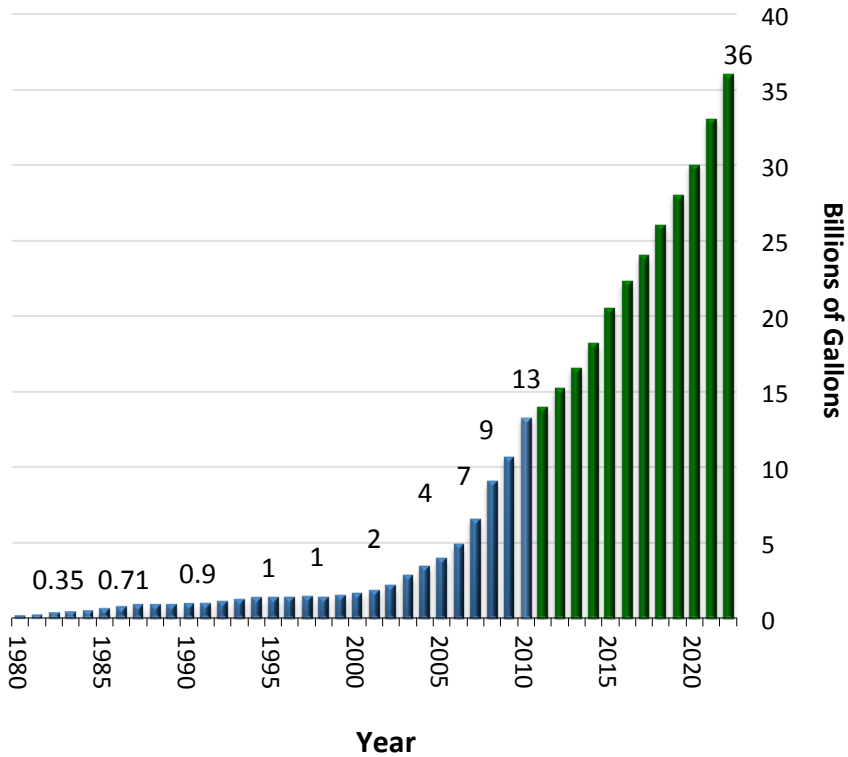


Global Ethanol Production

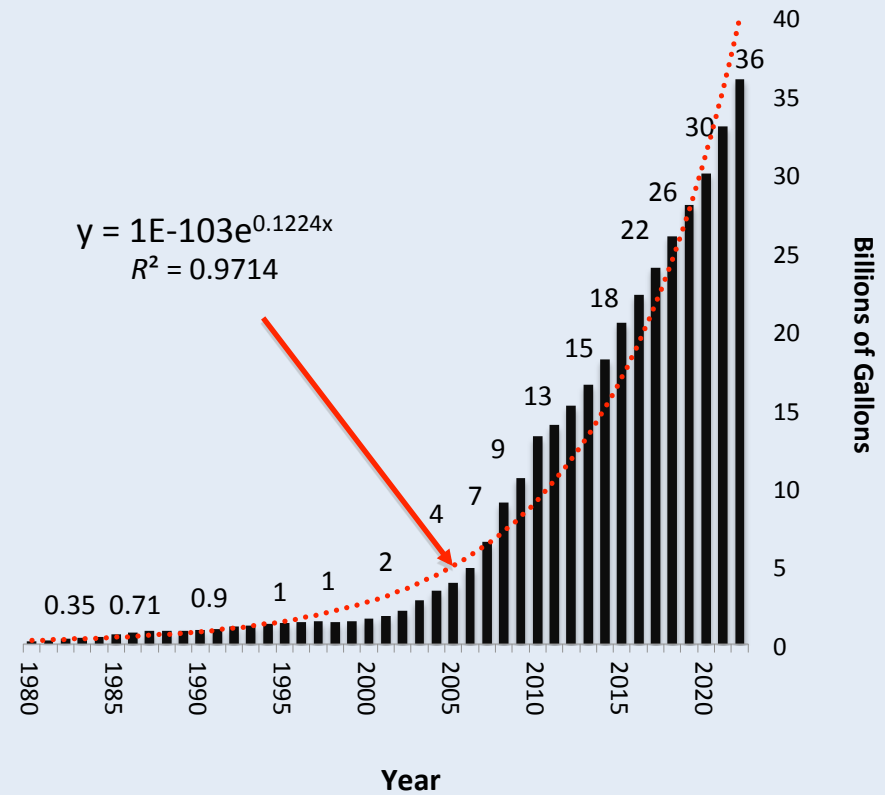
Top Five Countries (2013) Ethanol Production (millions of gallons/year) 1 Gal = 3.78 L



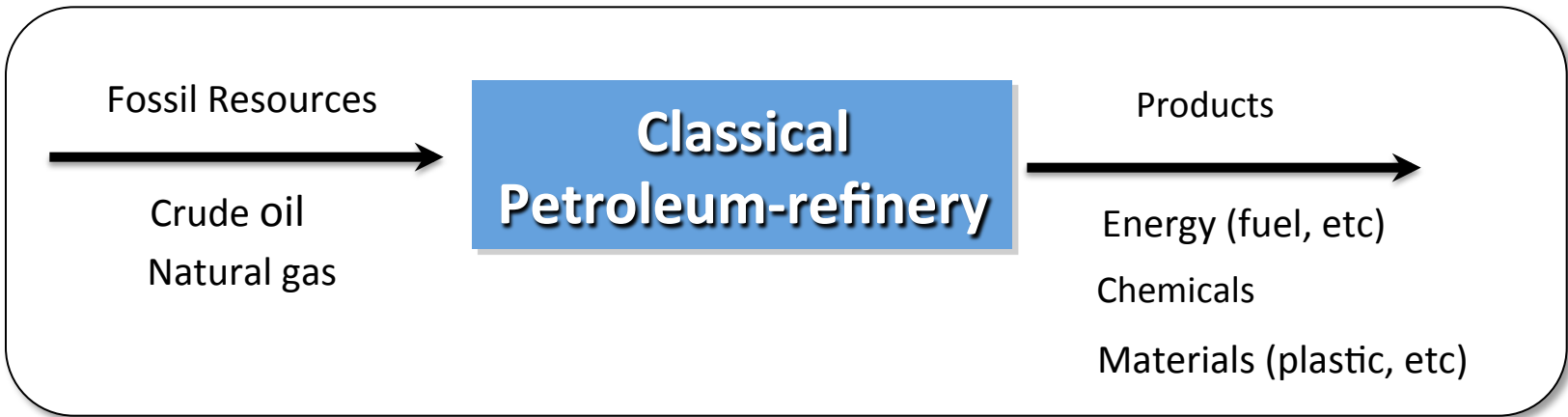
Market in USA



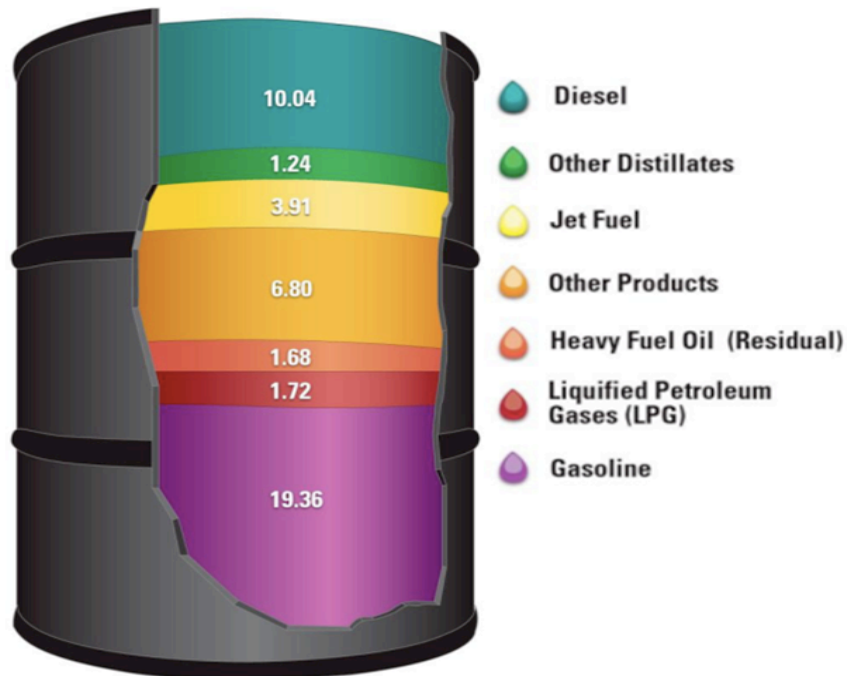
Non-linear Regression Analysis



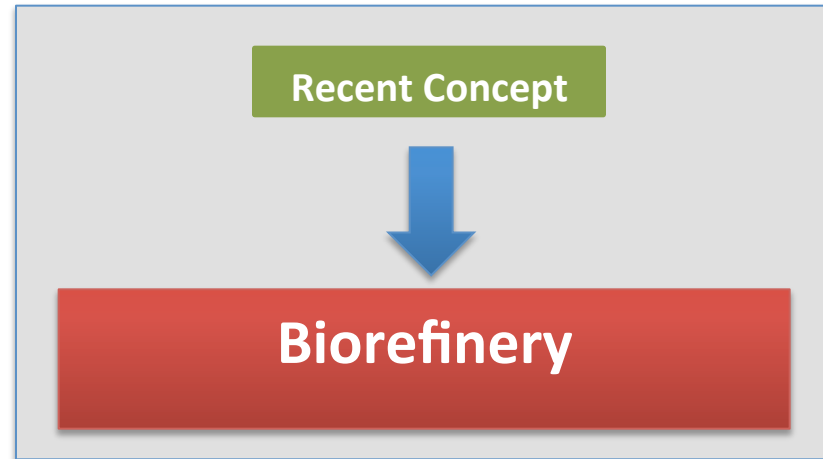
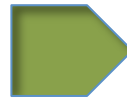
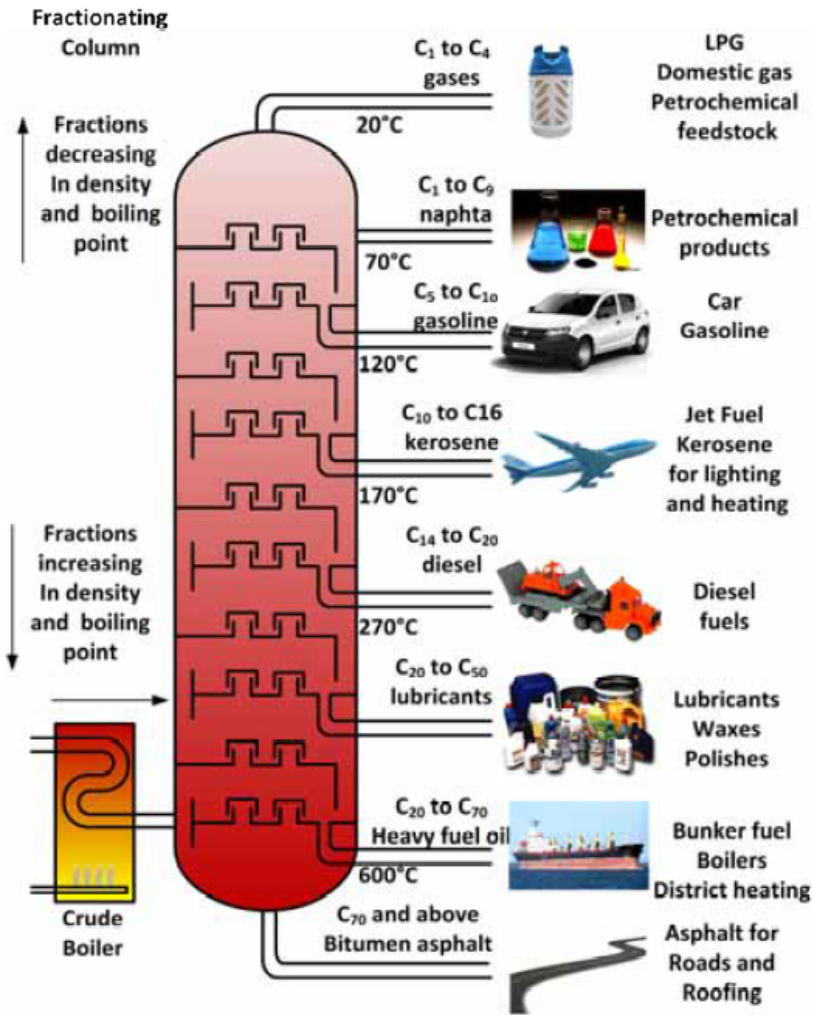
Héctor A. Ruiz et al. (2012). *Fuel*, 95 528-536



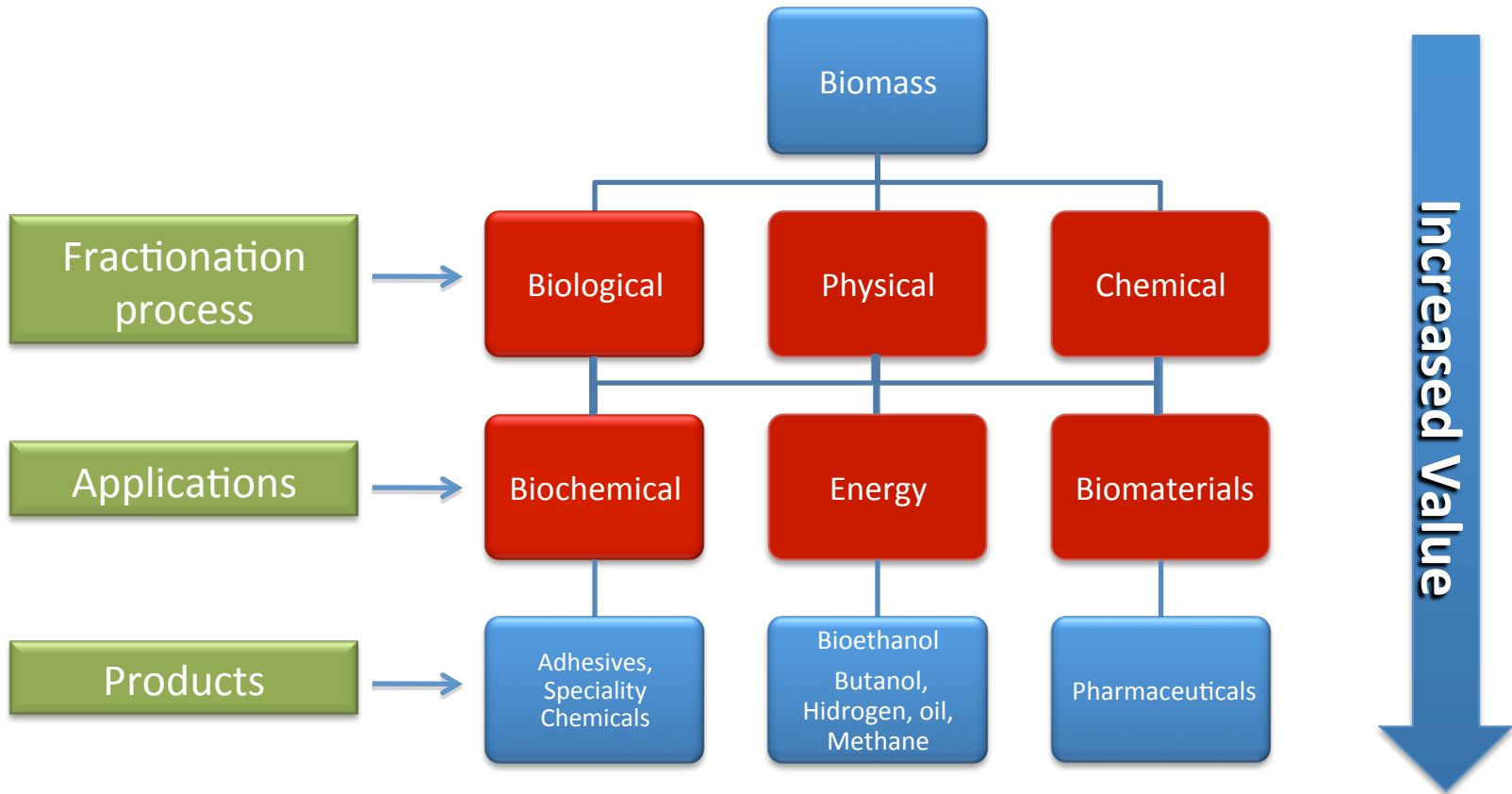
Products Made from a Barrel of Crude Oil (Gallons)



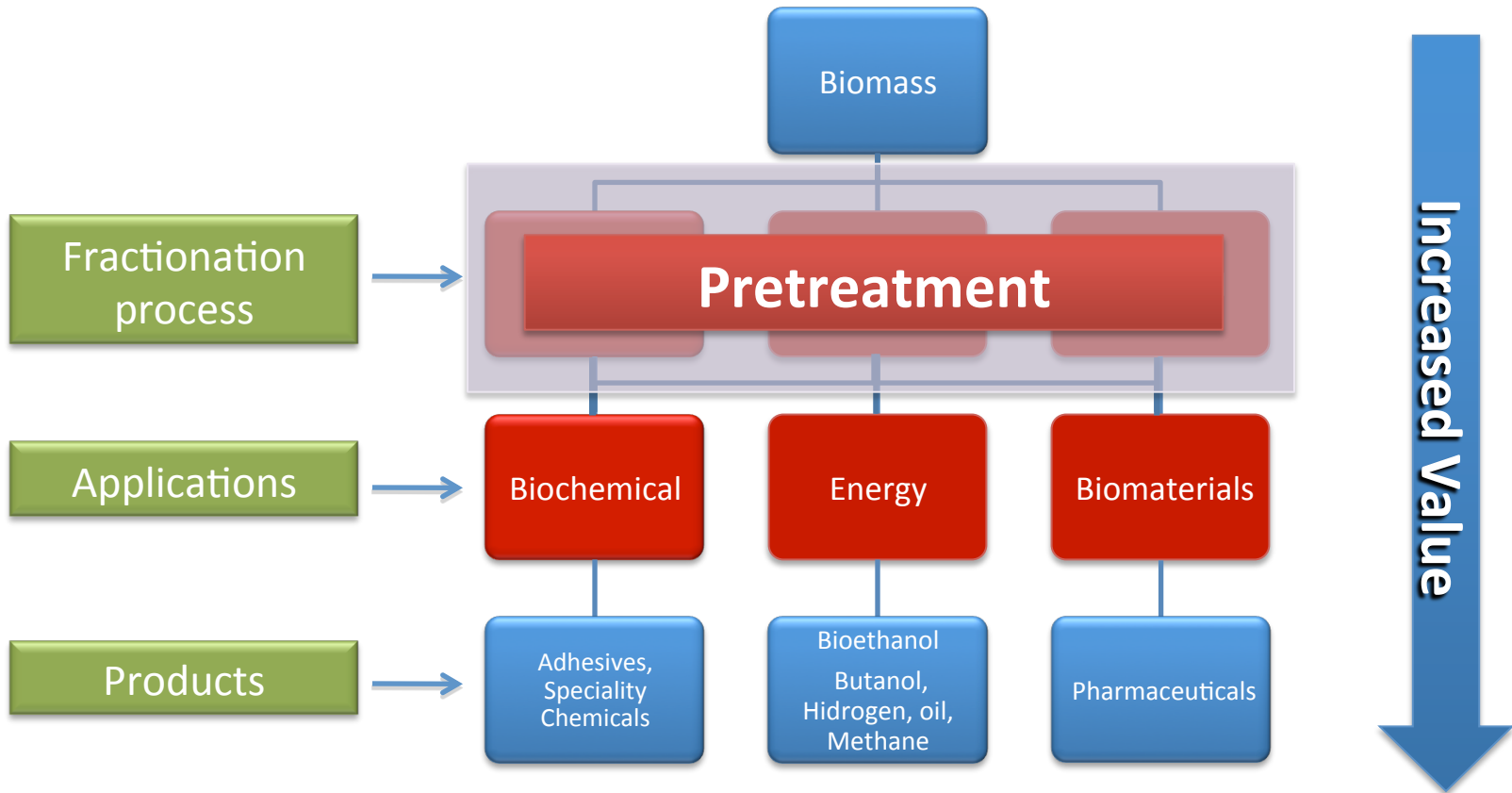
Fractional Distillation



Integrating of second and third generation biorefineries

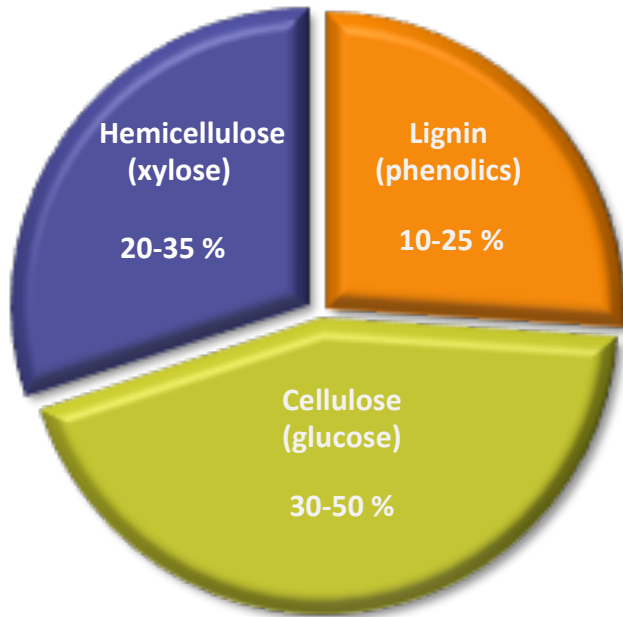


Integrating of second and third generation biorefineries

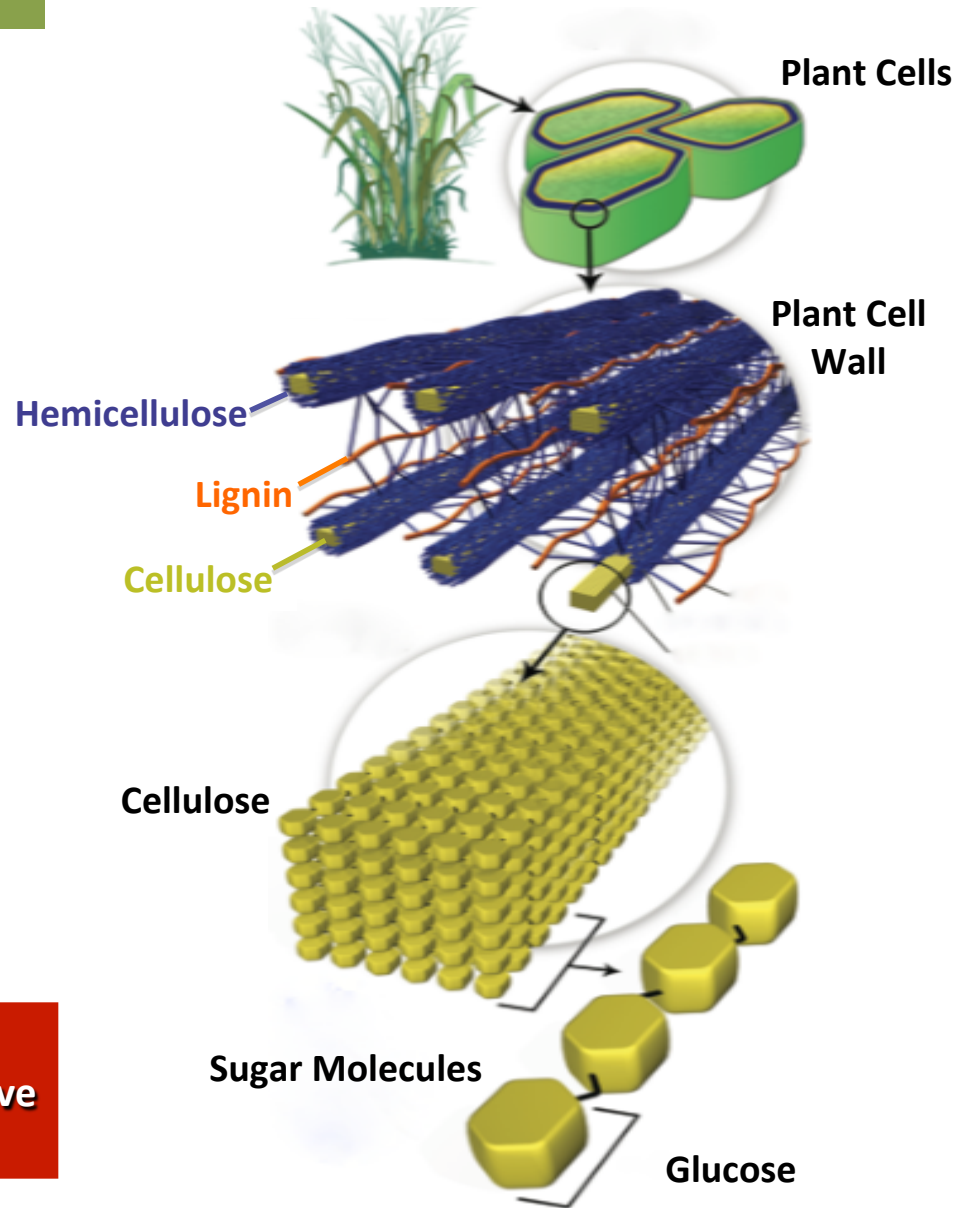


Second Generation of Bioethanol

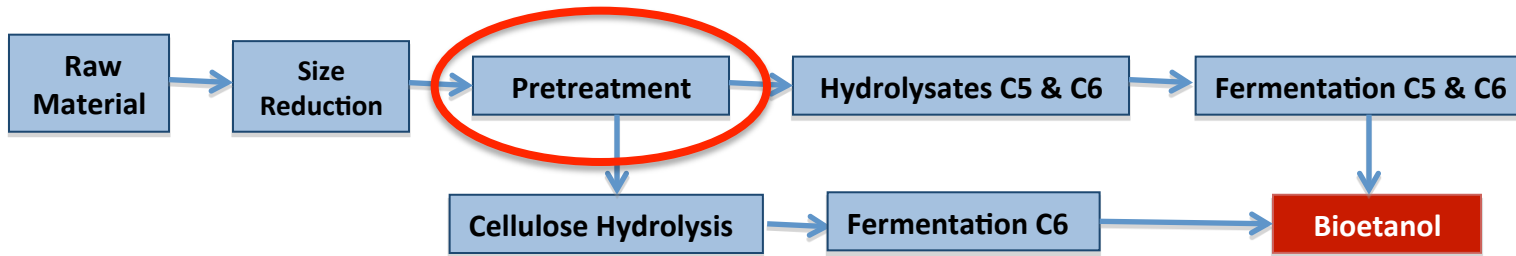
Lignocellulosic Materials (LCM) (Agricultural Residues)



Substrates
(wheat straw, corncobs, sugarcane bagasse, Agave bagasse, etc.)



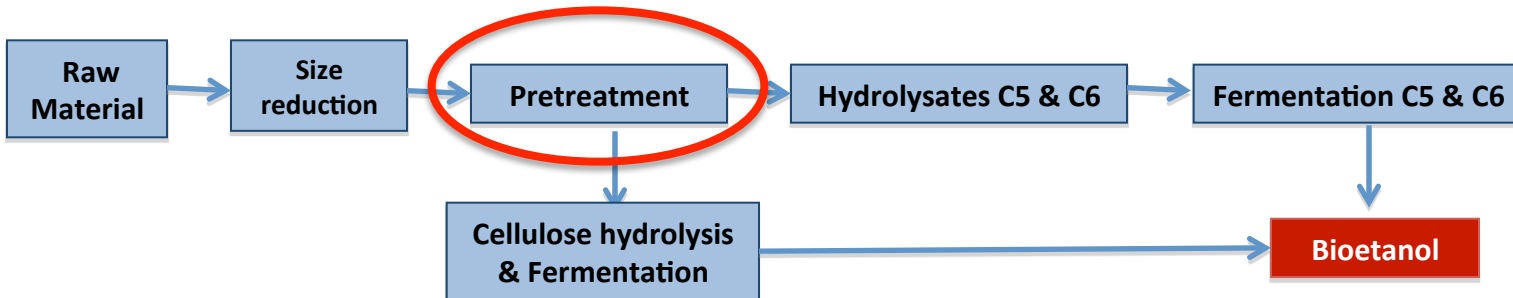
Separate Hydrolysis and Fermentation (SHF)



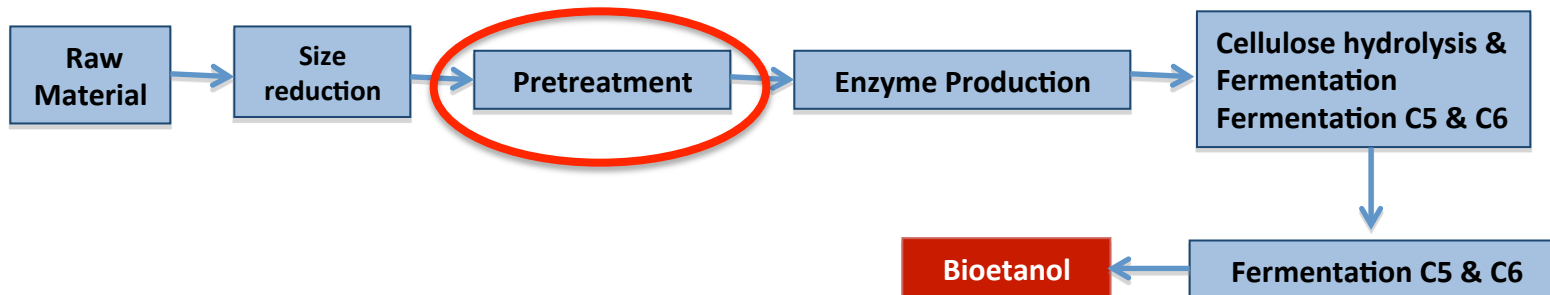
Simultaneous Saccharification and Fermentation (SSF)

or

Semi-simultaneous saccharification and fermentation (SSSF)

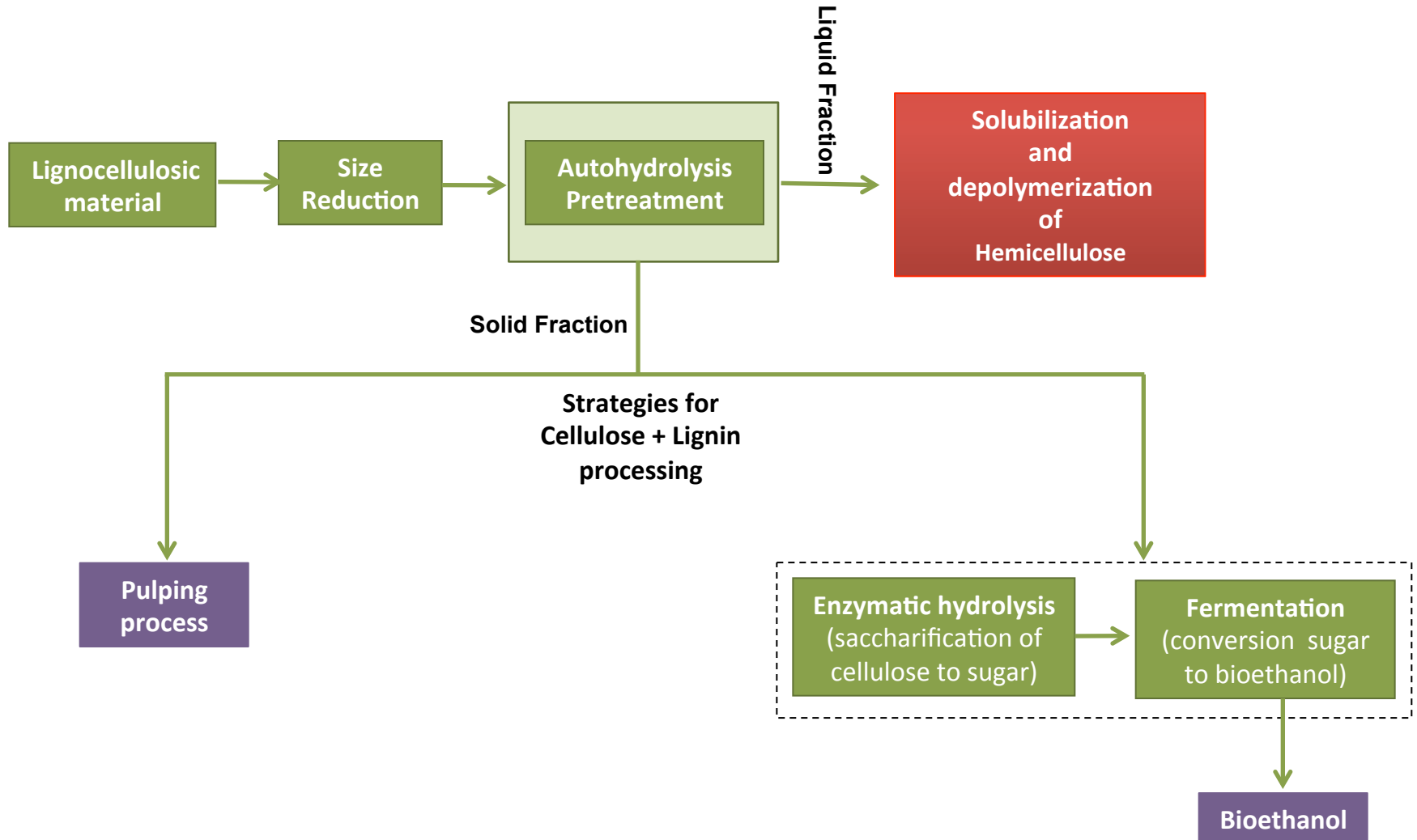


Consolidated Bioprocessing for Bioethanol Production



Fractionation of lignocellulosic material using hydrothermal processing

Our Work According to Integrated Biorefineries

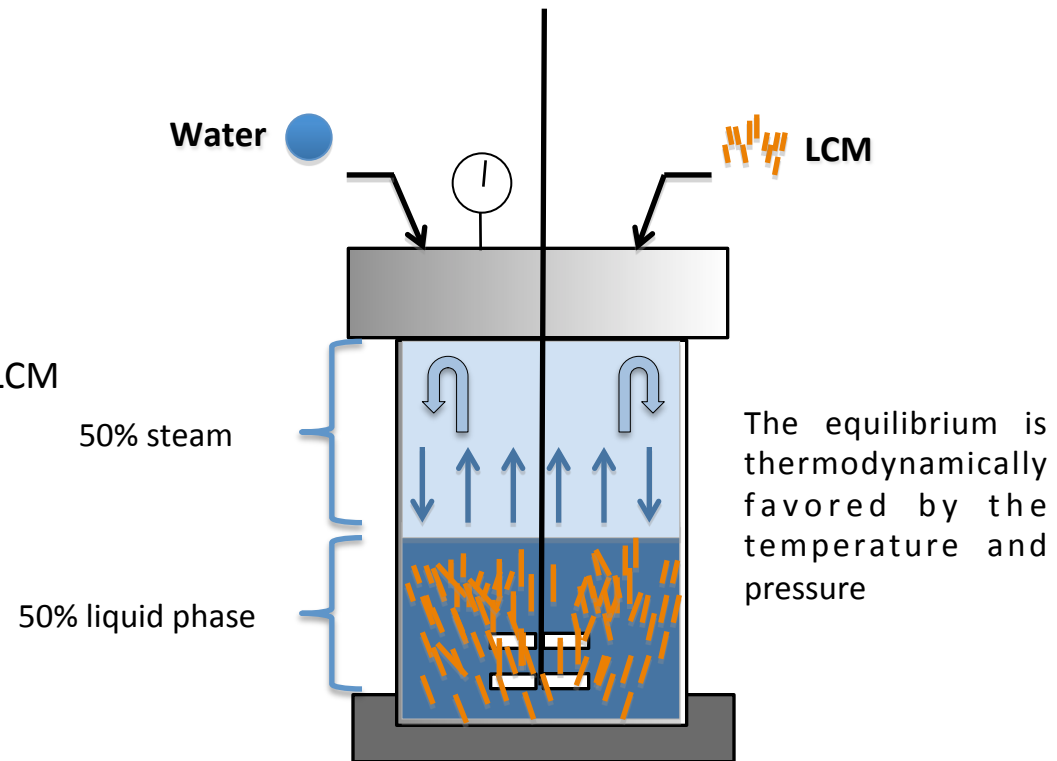


Fundamentals of Autohydrolysis Pretreatment

In this technology, water at high temperatures and pressures is applied on lignocellulosic materials for hydrolysis, extraction and structural modification: autohydrolysis, hydrothermal treatment, hot compressed water (HCW), hydrothermolysis, liquid-hot water (LHW), aqua solve process, aqueous processing and pressure-cooking in water.

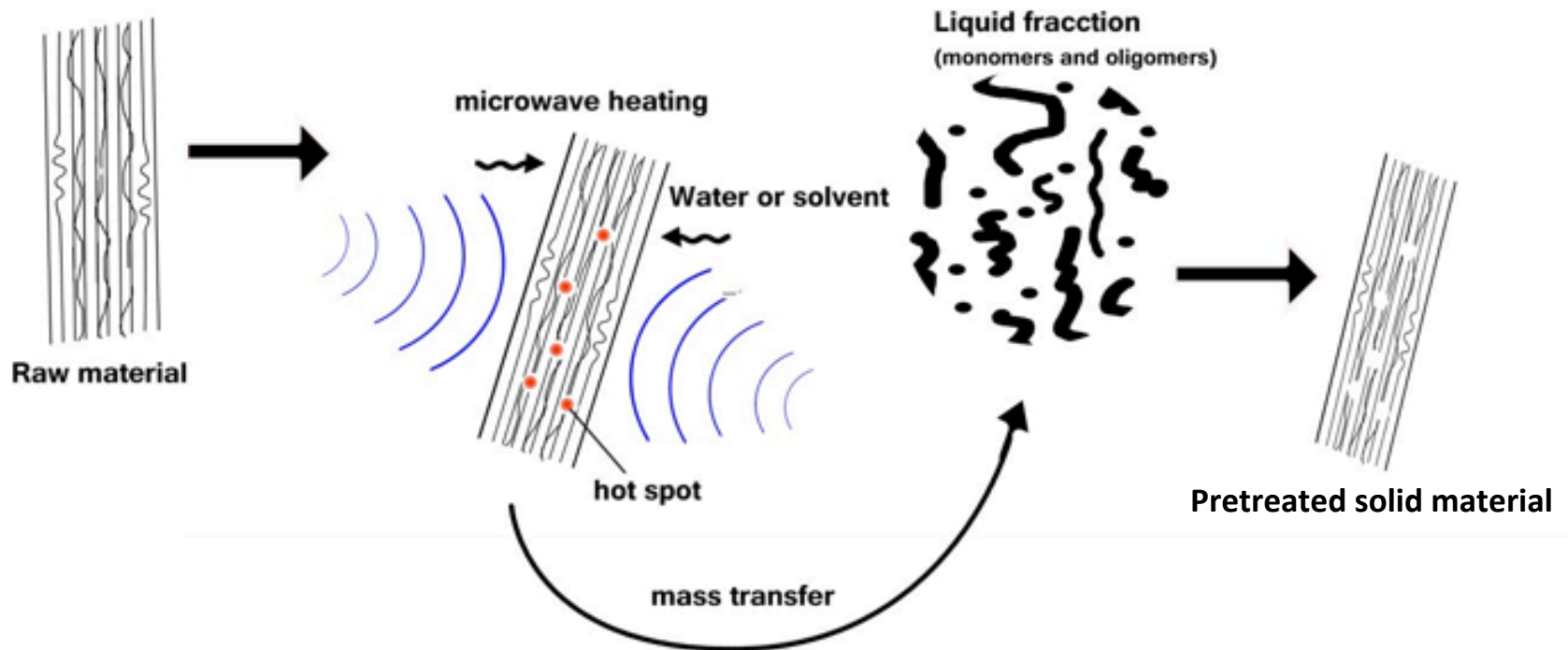
Advantages

- Environmentally friendly process
- Hemicellulose is solubilized and depolymerized
- Low by-product generation (inhibitors as furans)
- No chemicals other than water are necessary
- Caused relocalization of lignin on the surface of LCM



Microwave Pretreatment

Microwave radiation causes breakdown of the LCM via the collision molecular due to dielectric polarization, by increasing of the temperature selectively and non-homogenously in the more polar parts. Then some hot spots are created within the materials which generate their explosion due to the heat increase. The blast effect created between the particles by the method of heating improves relocation of crystalline structures of LCMs.



Heating (conduction, convection or radiation) in Autohydrolysis Pretreatment

The heating (conduction, convection or radiation) in the reactors can be performed by steam, fluidized sand baths, oil baths, electric heating jackets and microwave radiation to achieve fairly uniform heating as well as fast heat-up

Renewable and Sustainable Energy Reviews 21 (2013) 35–51



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Renewable and Sustainable Energy Reviews

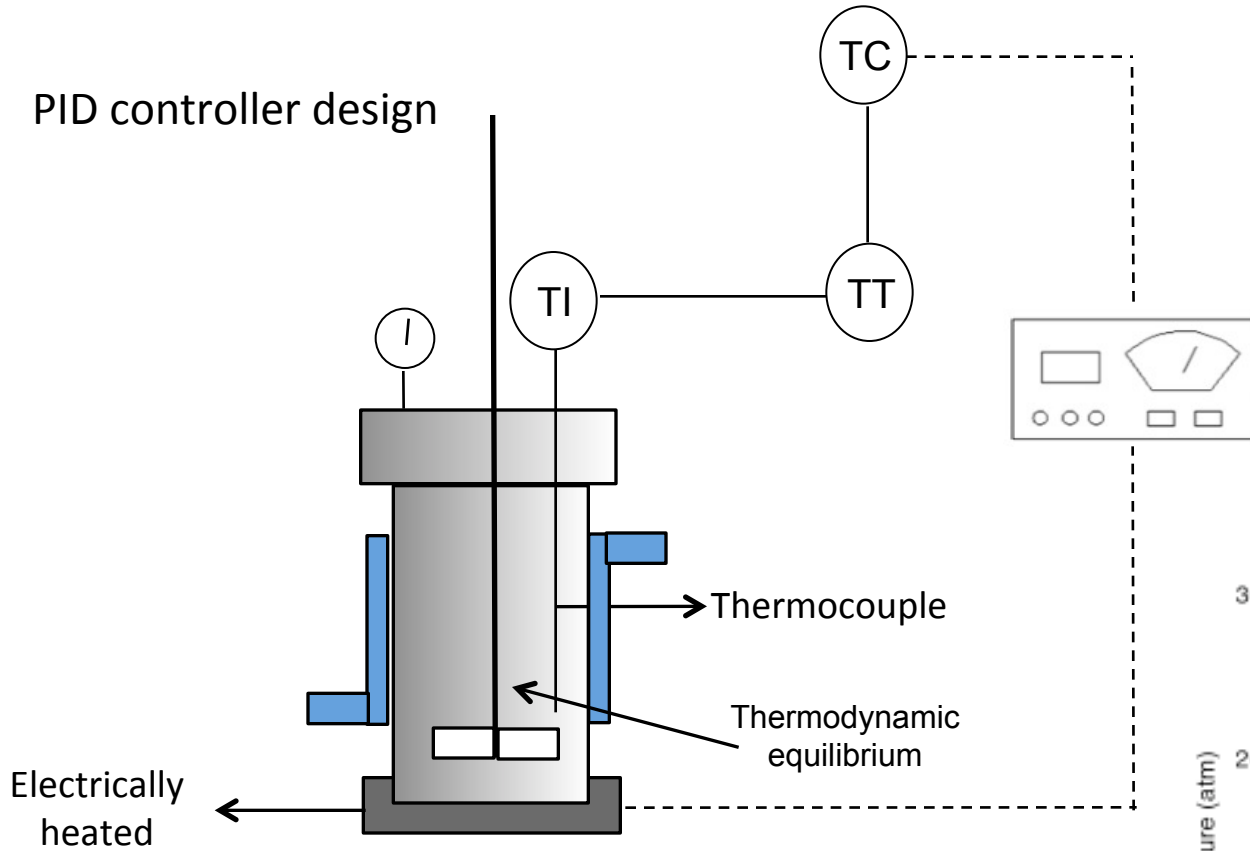
journal homepage: www.elsevier.com/locate/rser



Hydrothermal processing, as an alternative for upgrading agriculture residues and marine biomass according to the biorefinery concept: A review
Héctor A. Ruiz*, Rosa M. Rodríguez-Jasso, Bruno D. Fernandes, António A. Vicente, José A. Teixeira

Fundamentals of Autohydrolysis Pretreatment

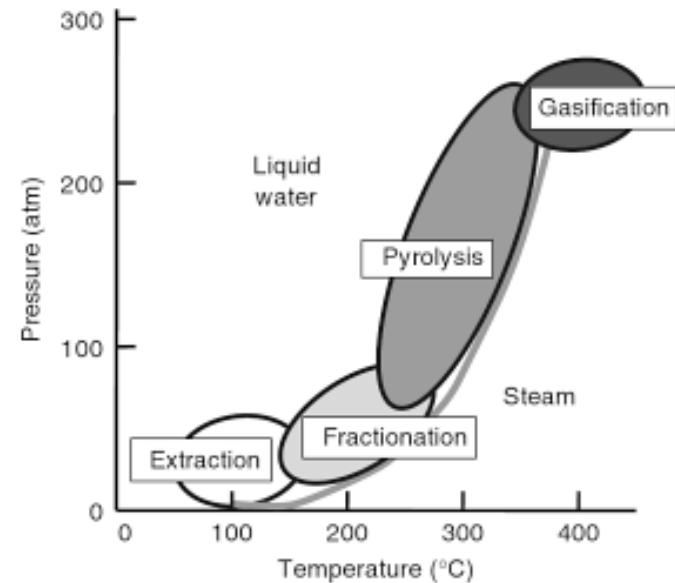
PID controller design



Other heating sources

- Steam
- Microwave Radiation

- Autoionization of water into hydronium ions H_3O^+ as catalyst
- Acetic acid from acetyl groups of hemicellulose



Heating and Cooling Temperature Profiles in Autohydrolysis Process

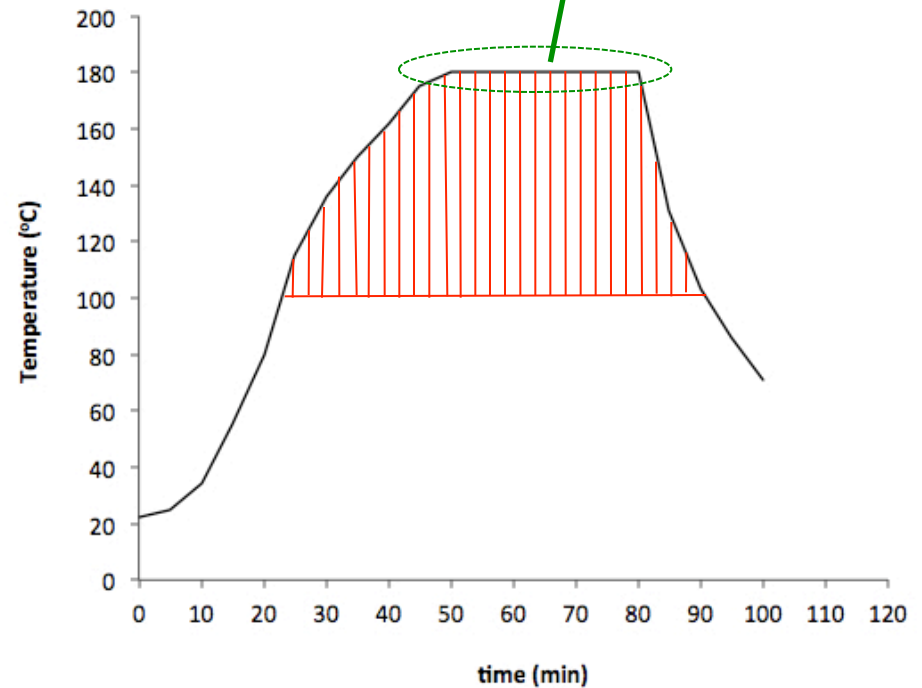
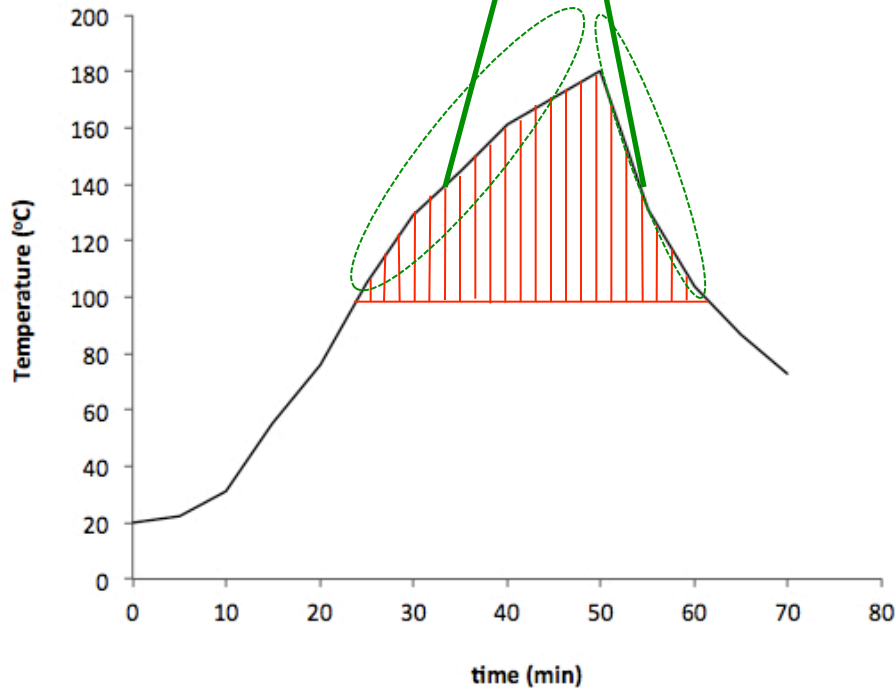
$$\log R_0 = \log [R_{0 \text{ Heating}} + R_{0 \text{ Cooling}}]$$

$$\log R_0 = \left[\int_0^{t_{MAX}} \frac{T(t) - 100}{\omega} dt + \int_{t_{MAX}}^{t_F} \frac{T'(t) - 100}{\omega} dt \right]$$

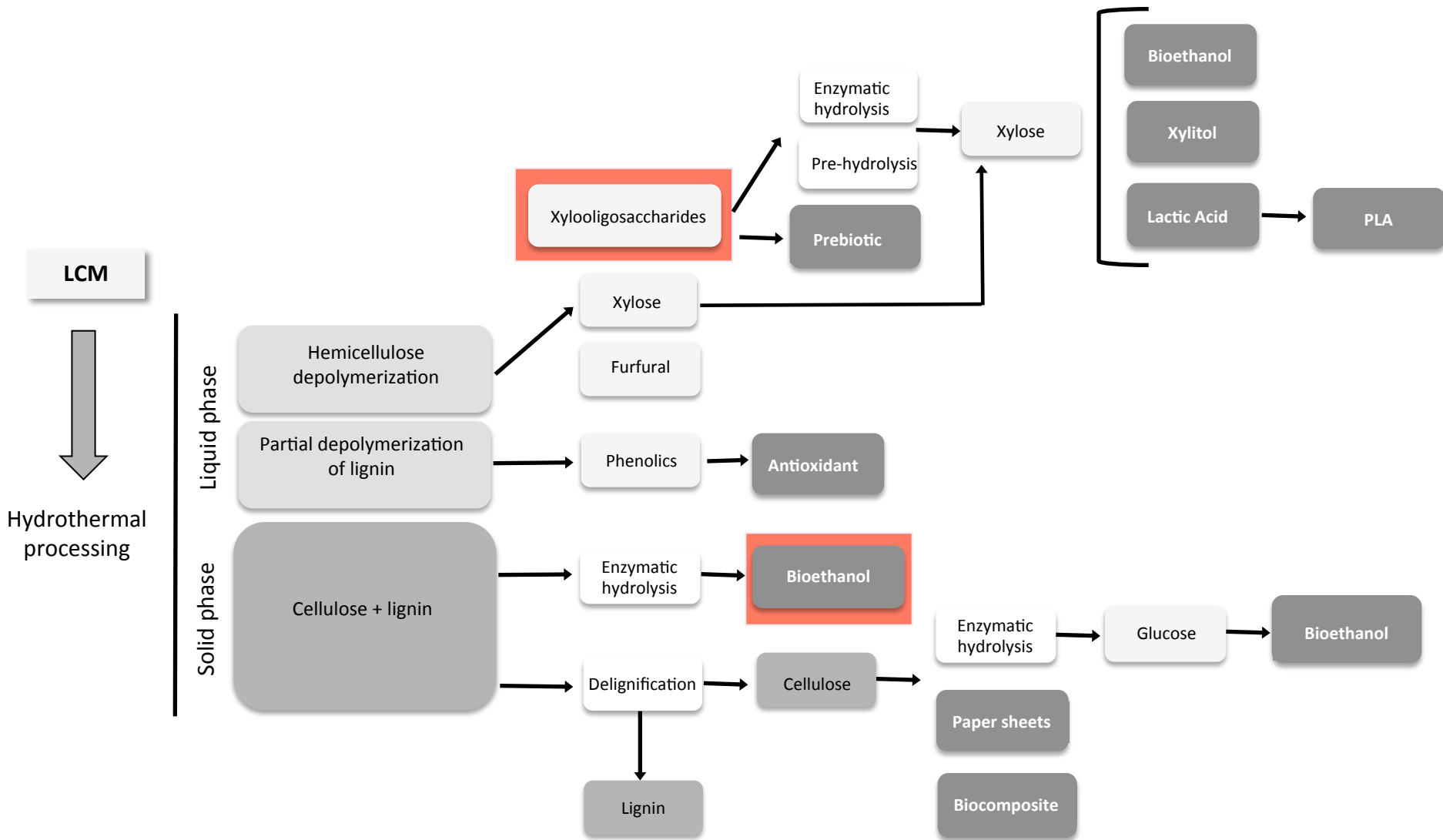
non-isothermal heating regimen section

$$\text{Log} (R_0) = \int_0^t \exp \left[\frac{T - 100}{14.75} \right] dt$$

isothermal heating regimen section



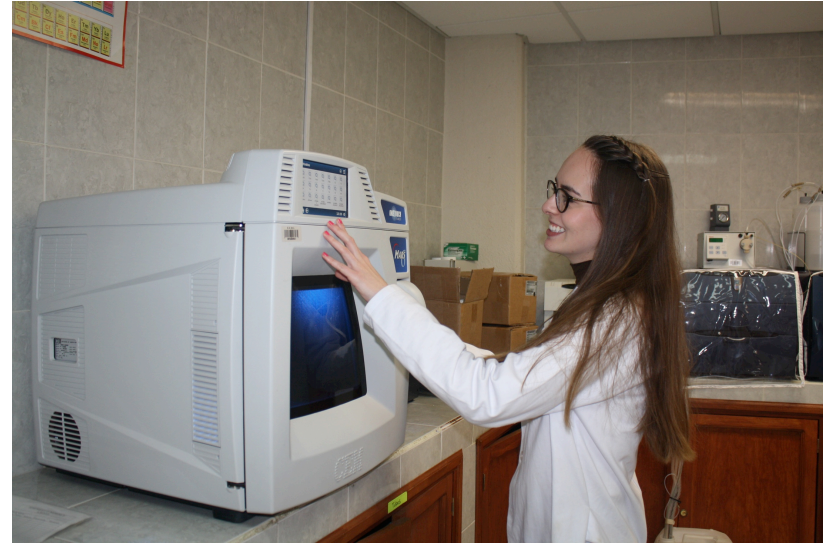
Integrated Biorefineries Platform Using Hydrothermal Process



Our Work According to Integrated Biorefineries using using Corn residues



conduction- convection

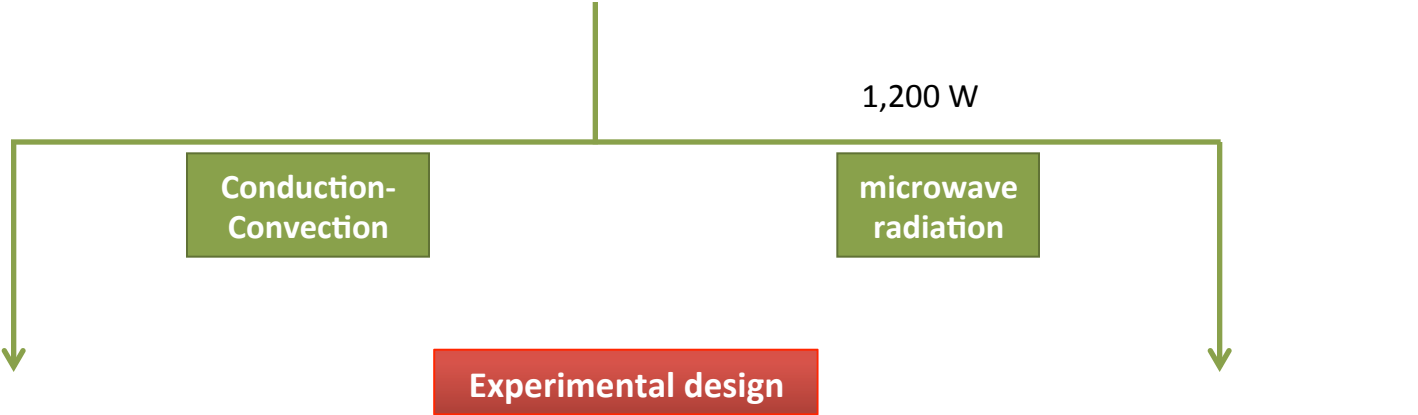


microwave radiation

**Corn residues
(cobs and stover)**



Autohydrolysis Pretreatment: Conduction- Convection and microwave radiation on corn residues



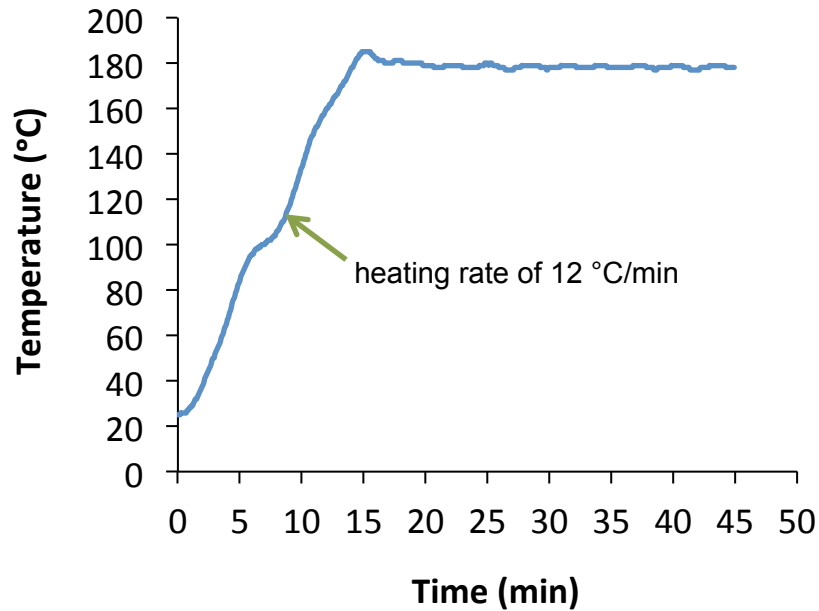
Assay	time (min)	Temperature (°C)
1	20	160
2	20	200
3	60	160
4	60	200
5	40	180
6	40	180
7	20	180
8	60	180
9	40	160
10	40	200



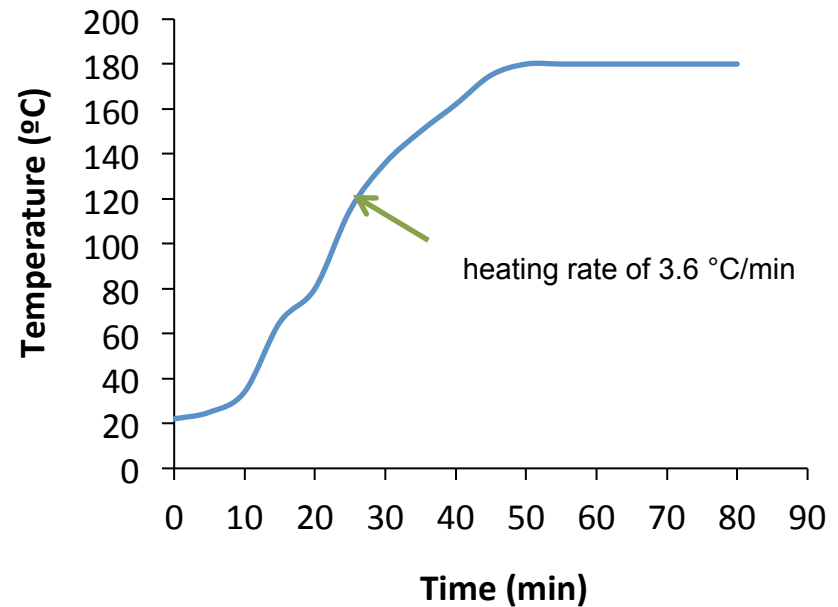
Oligomers from hemicellulose (g/ 100 g r.m) in dry basis

Heating profiles

Microwave radiation



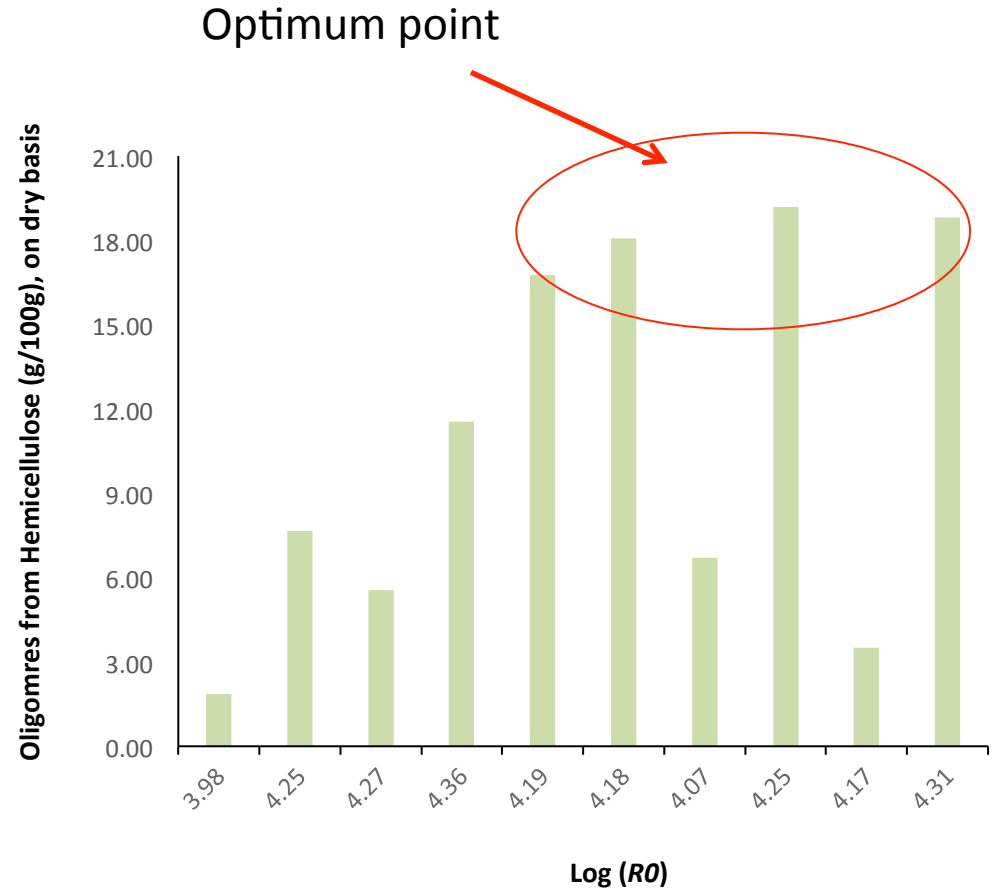
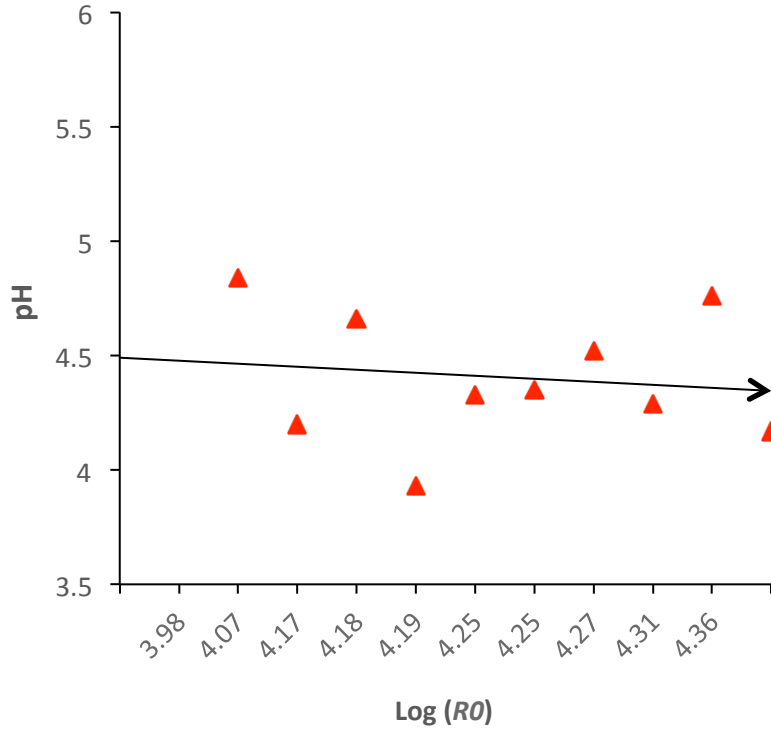
Conduction-Convection



Chemical Characterization (g/100 g), on dry basis

R₀ (Factor de severidad)	CELULOSA		HEMICELULOSA		LIGNINA KLASON	
	MH	CH	MH	CH	MH	CH
3.98 (150/10)	36.43±1.34	38.72±0.32	20.55±0.88	23.49±0.67	19.09±0.67	15.69±0.12
4.31 (150/30)	42.16±0.50	42.84±0.57	17.06±0.68	20.17±0.65	20.26±0.65	16.89±0.42
4.17 (150/50)	47.17±1.01	45.16±1.13	9.93±0.21	18.07±0.23	23.02±0.23	18.01±0.75
4.19 (165/10)	45.09±0.03	43.38±1.58	11.97±0.31	18.49±0.75	21.75±0.75	19.04±0.64
4.25 (165/30)	56.77±0.35	59.70±0.79	6.02±0.40	8.89±0.16	23.82±0.16	24.65±0.41
4.27 (165/50)	61.49±1.21	61.75±1.27	2.78±0.10	3.52±0.12	24.71±0.12	27.42±0.68
4.07 (180/10)	59.48±0.15	61.45±0.25	2.63±0.39	4.11±0.13	26.91±0.13	25.45±0.40
4.18 (180/30)	64.67±0.24	62.60±0.02	0.84±0.15	1.81±0.09	30.40±0.09	31.81±0.13
4.36(180/50)	61.74±1.23	63.04±0.94	0.27±0.02	0.00±0.0	33.23±0.00	34.95±0.03

Results of Autohydrolysis: Conduction- Convection



Optimization of Autohydrolysis for oligomers from Hemicellulose

This optimum point was determined using the Hessian matrix method

$$\text{Oligomers} = -1038 + 12.3t - 0.04t^2 + 1.2T - 0.012t^2 - 0.0028tT$$

$$\frac{\partial z}{\partial x} = 12.31225264 - 0.0027284y - 0.07284911x$$

$$\frac{\partial z}{\partial y} = 1.24011046 - 0.02301808y - 0.0027284x$$

$$\frac{\partial^2 z}{\partial x^2} = -0.07284911 \quad \frac{\partial^2 z}{\partial y^2} = -0.02301808$$

$$\frac{\partial^2 z}{\partial x \partial y} = -0.0027284 \quad \frac{\partial^2 z}{\partial y \partial x} = -0.0027284$$

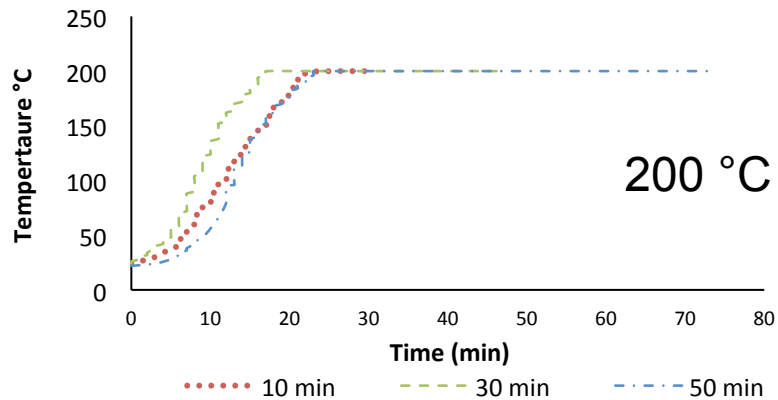
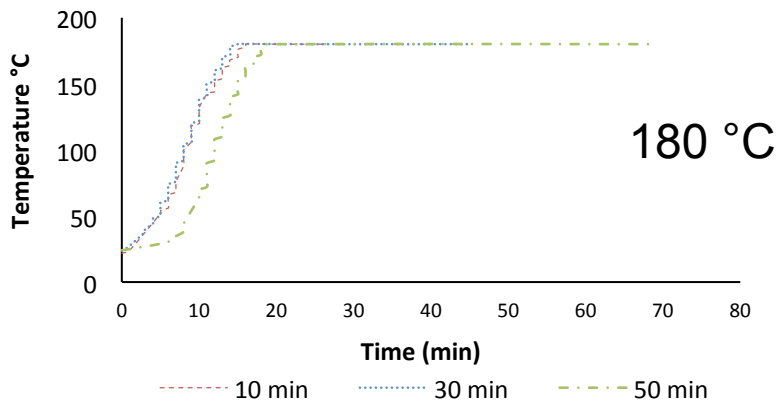
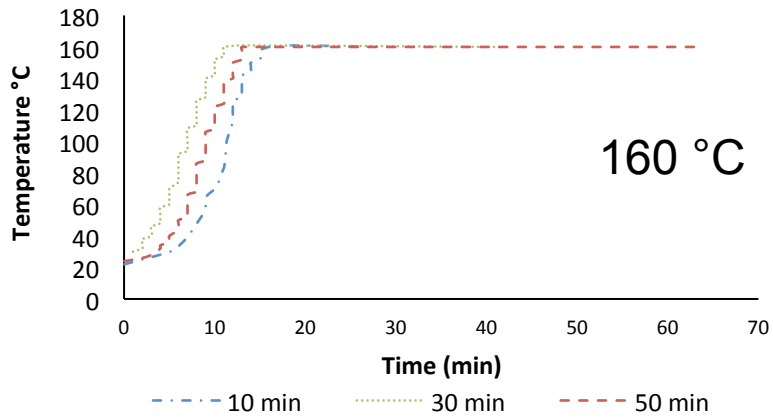
$$H(x, y) = \begin{bmatrix} \frac{\partial^2 z}{\partial x^2} & \frac{\partial^2 z}{\partial x \partial y} \\ \frac{\partial^2 z}{\partial y \partial x} & \frac{\partial^2 z}{\partial y^2} \end{bmatrix} = \begin{bmatrix} -0.07284911 & -0.0027284 \\ -0.0027284 & -0.02301808 \end{bmatrix}$$

$$H(x, y) = (-0.07284911)(-0.02301808) - (-0.0027284)(-0.0027284) = 0.0016694$$

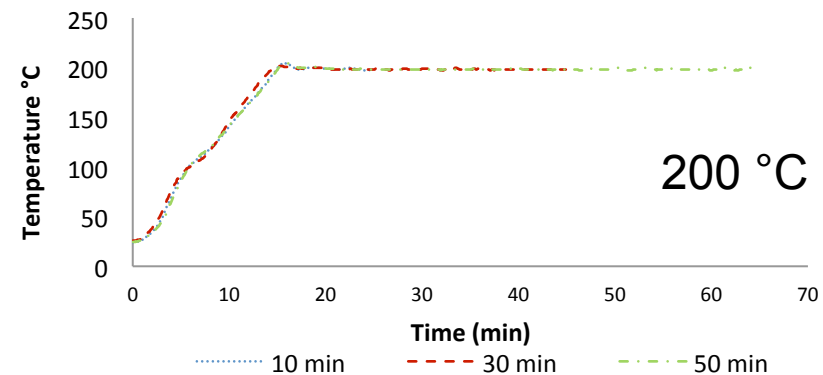
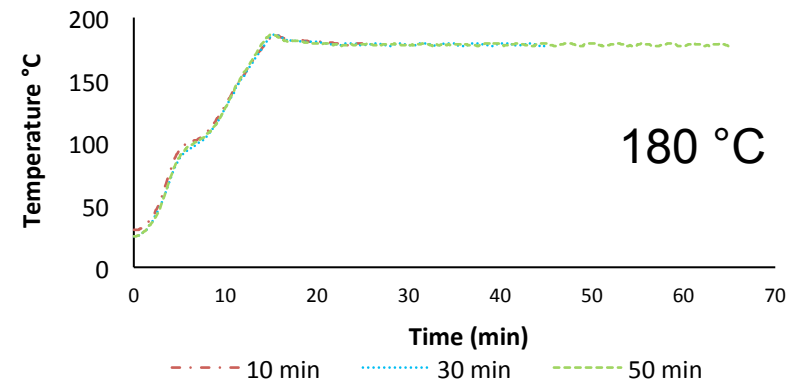
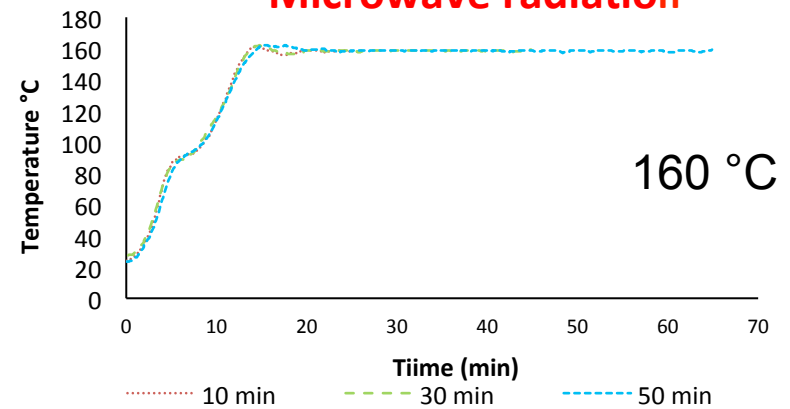
(1) Optimum point for Conduction- Convection = 18.98 g /100 g

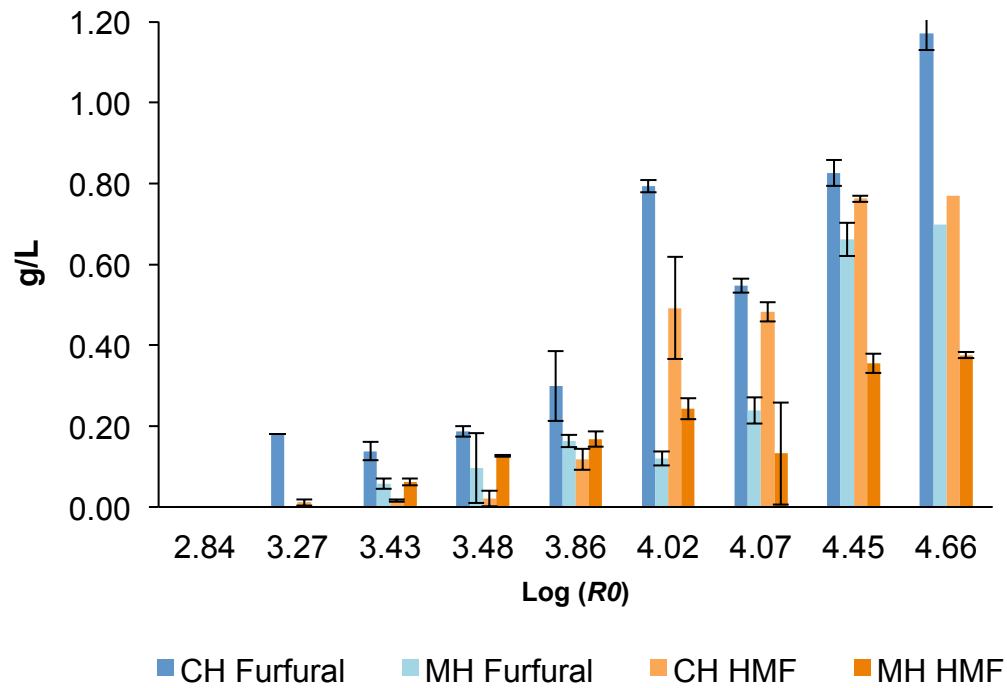
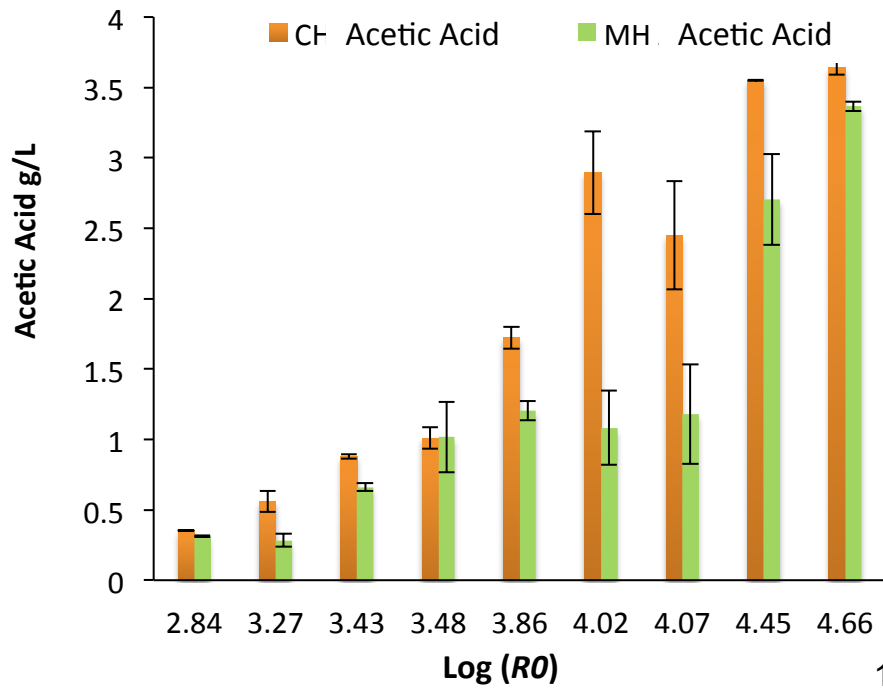
(2) Optimum point for Microwave radiation = 16.96 g /100 g

Conduction- Convection



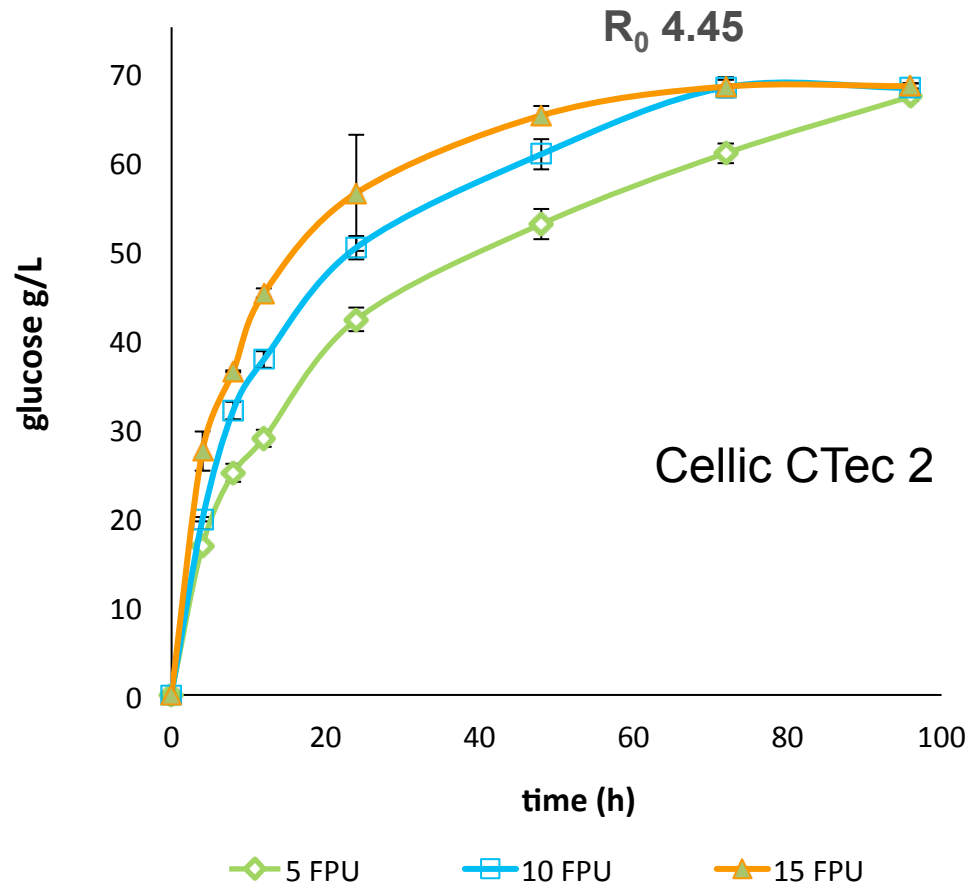
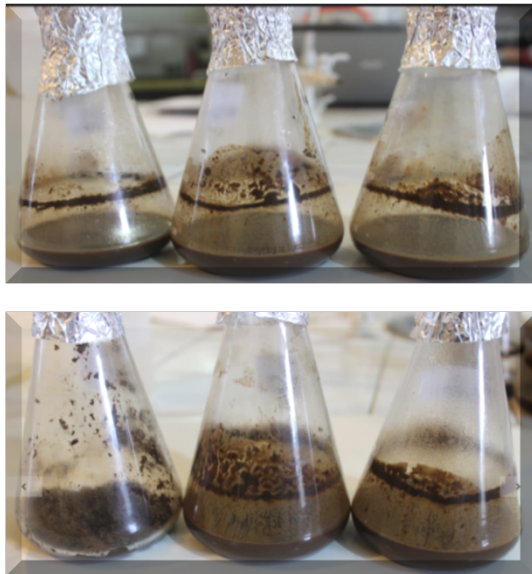
Microwave radiation





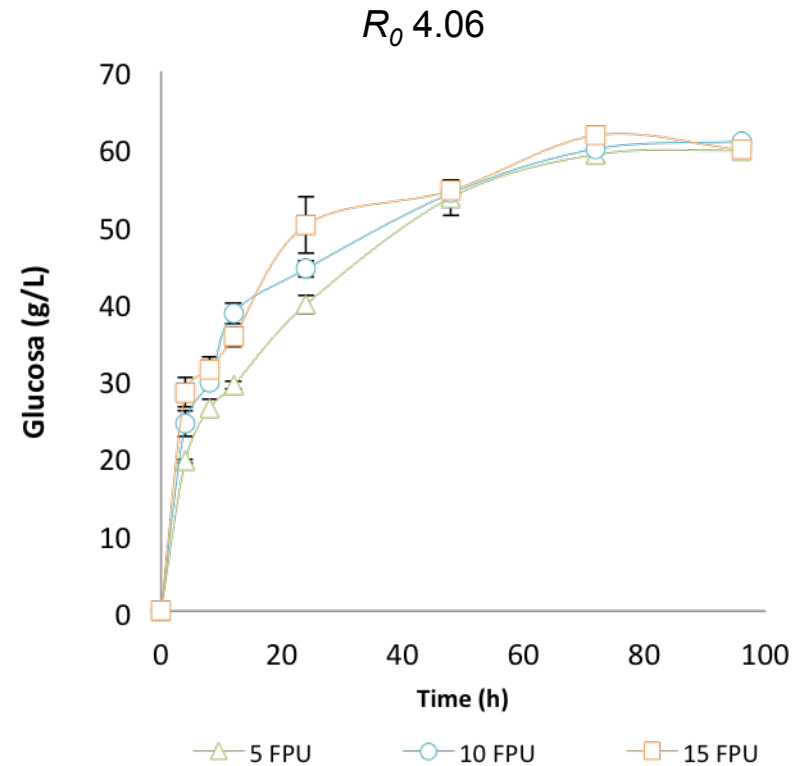
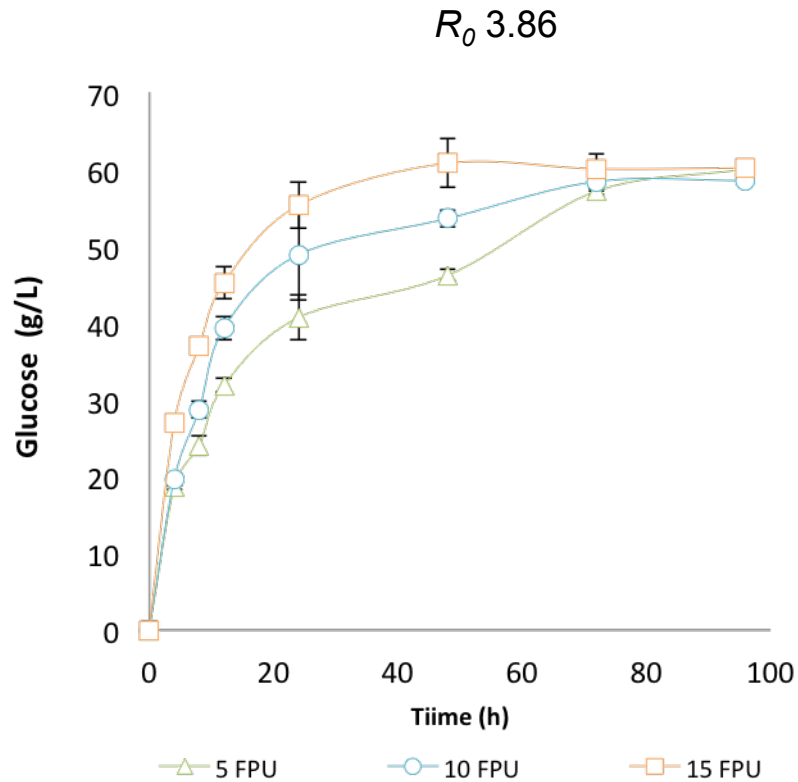
Enzymatic hydrolysis – Microwave Radiation

Cellic CTec 2



Enzymatic hydrolysis – Conduction-Convection

Cellic CTec 2





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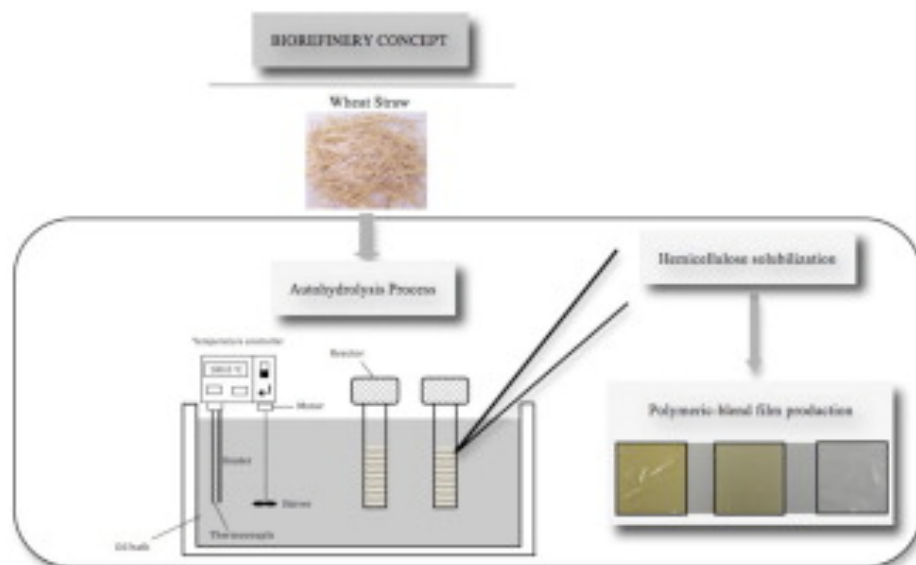


Biorefinery valorization of autohydrolysis wheat straw hemicellulose to be applied in a polymer-blend film

Héctor A. Ruiz*, Miguel A. Cerqueira*, Hélder D. Silva, Rosa M. Rodríguez-Jasso, António A. Vicente*, José A. Teixeira

The incorporation of hydrothermal extracted hemicellulose improved the physical properties of: κ -carrageenan/locust bean gum polymeric films

Graphical abstract

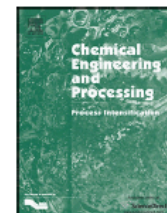




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Chemical Engineering and Processing: Process Intensification

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Non-alkaline solubilization of arabinoxylans from destarched wheat bran using hydrothermal microwave processing and comparison with the hydrolysis by an endoxylanase



Mario Aguedo^{a,*}, Héctor A. Ruiz^b, Aurore Richel^a

^a *Laboratory of Biological and Industrial Chemistry, Gembloux Agro-Bio Tech – University of Liège, Passage des Déportés 2, 5030 Gembloux, Belgium*

^b *Biorefinery Group, Food Research Department, School of Chemistry, Autonomous University of Coahuila, Blvd. V. Carranza e Ing. José Cárdenas Valdés, 25280 Saltillo, Coahuila, Mexico*

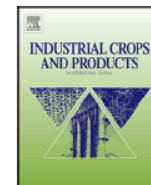
Industrial Crops and Products 66 (2015) 305–311



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Industrial Crops and Products

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Use of wheat bran arabinoxylans in chitosan-based films:
Effect on physicochemical properties



Maria J. Costa^{a,*}, Miguel A. Cerqueira^{a,*}, Héctor A. Ruiz^b, Christian Fournies^c,
Aurore Richel^d, António A. Vicente^a, José A. Teixeira^a, Mario Aguedo^d

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^b *Biorefinery Group, Food Research Department, School of Chemistry, Autonomous University of Coahuila, Blvd. V. Carranza e Ing. José Cárdenas Valdés, 25280 Saltillo, Coah., Mexico*

^c *Cosucra Groupe Warcoing S.A., Rue de la Sucrierie 1, 7740 Warcoing, Belgium*

^d *Laboratory of Biological and Industrial Chemistry, University of Liège – Gembloux Agro-Bio Tech, Passage des Déportés 2, 5030 Gembloux, Belgium*

In general, autohydrolysis (Hydrothermal processing) can be considered a promising technology for the biorefinery concept, obtaining in an only step the fractionation of lignocellulosic materials and products with high added-value according to the biorefinery concept.

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