

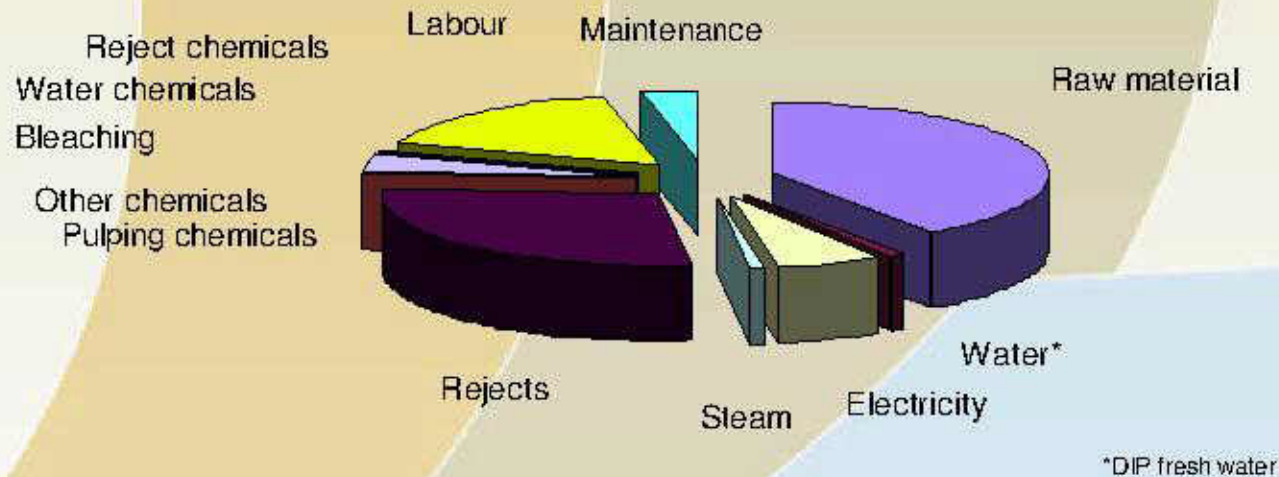
# Factors defining tissue DIP concept: end product demands, raw material and operational costs



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Sales & Process Manager  
South America

# DIP cost analysis for tissue (example)

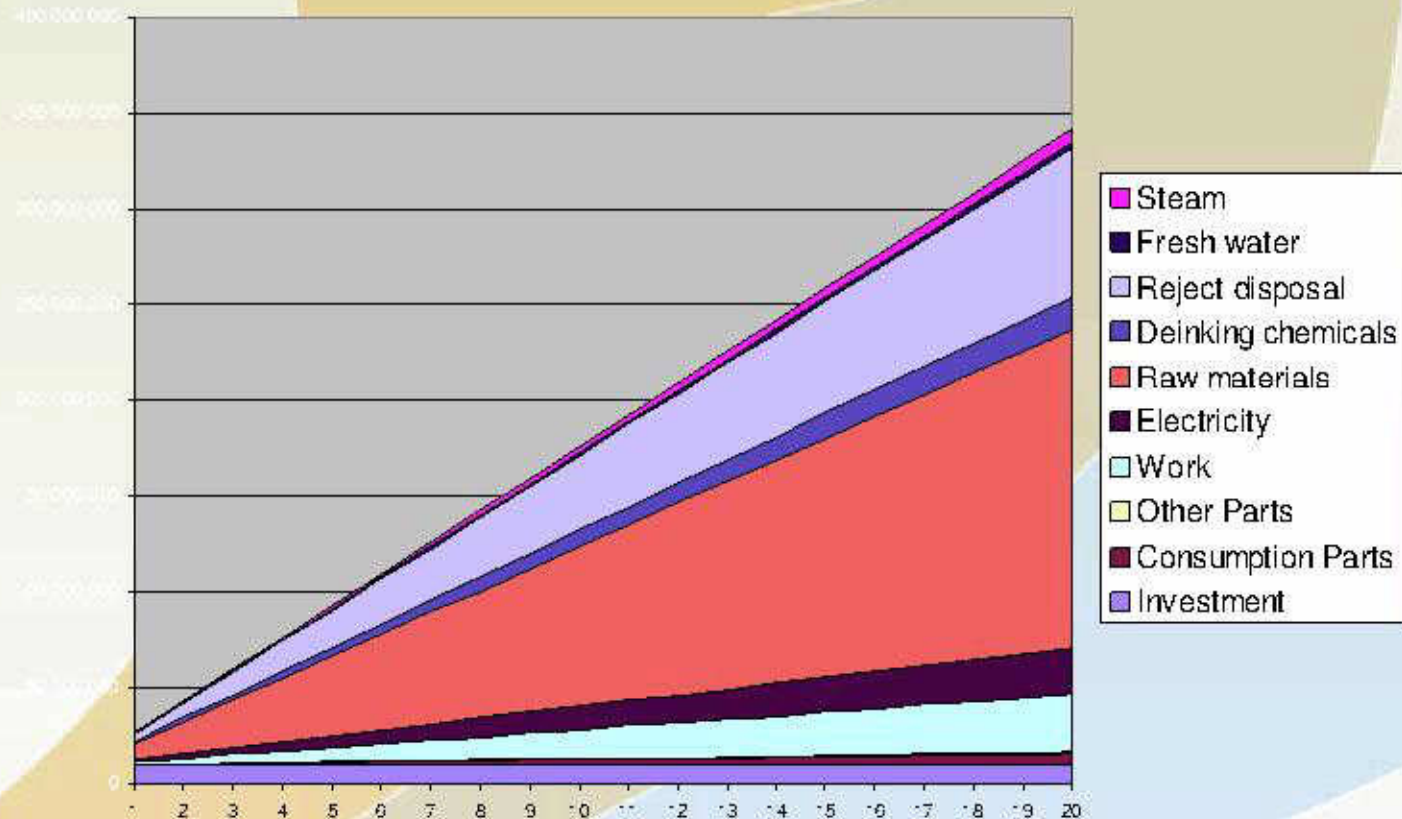
## End product demands, raw material & operational costs



- **Costs variables are typically mill specific (final product, raw material, labour, electricity, water, reject treatment/disposal)**
- **By technology and concept solutions we can affect the total costs = investment + operational costs**

# Life-cycle costs (example)

**Total costs = Investment + Operational Costs**



**Dedication for life-time cost reduction! => RTD, service, performance studies**

# Yield as a Function of Ash Contents

$$\text{Yield (\%)} = 100 * \frac{A_{\text{production}}}{F_{\text{production}}}$$

Measurement of production.

$$\text{Yield (\%)} = \frac{100 * (R_{\text{ash}} - F_{\text{ash}})}{(R_{\text{ash}} - A_{\text{ash}})}$$

Measurement of ash content gives repeatable result.

Feed ash content (%)  
=  $F_{\text{ash}}$



Accept ash content (%)  
=  $A_{\text{ash}}$

Reject ash content (%) =  $R_{\text{ash}}$

For the total yield calculation, the outthrows of the pulper must take into consideration.



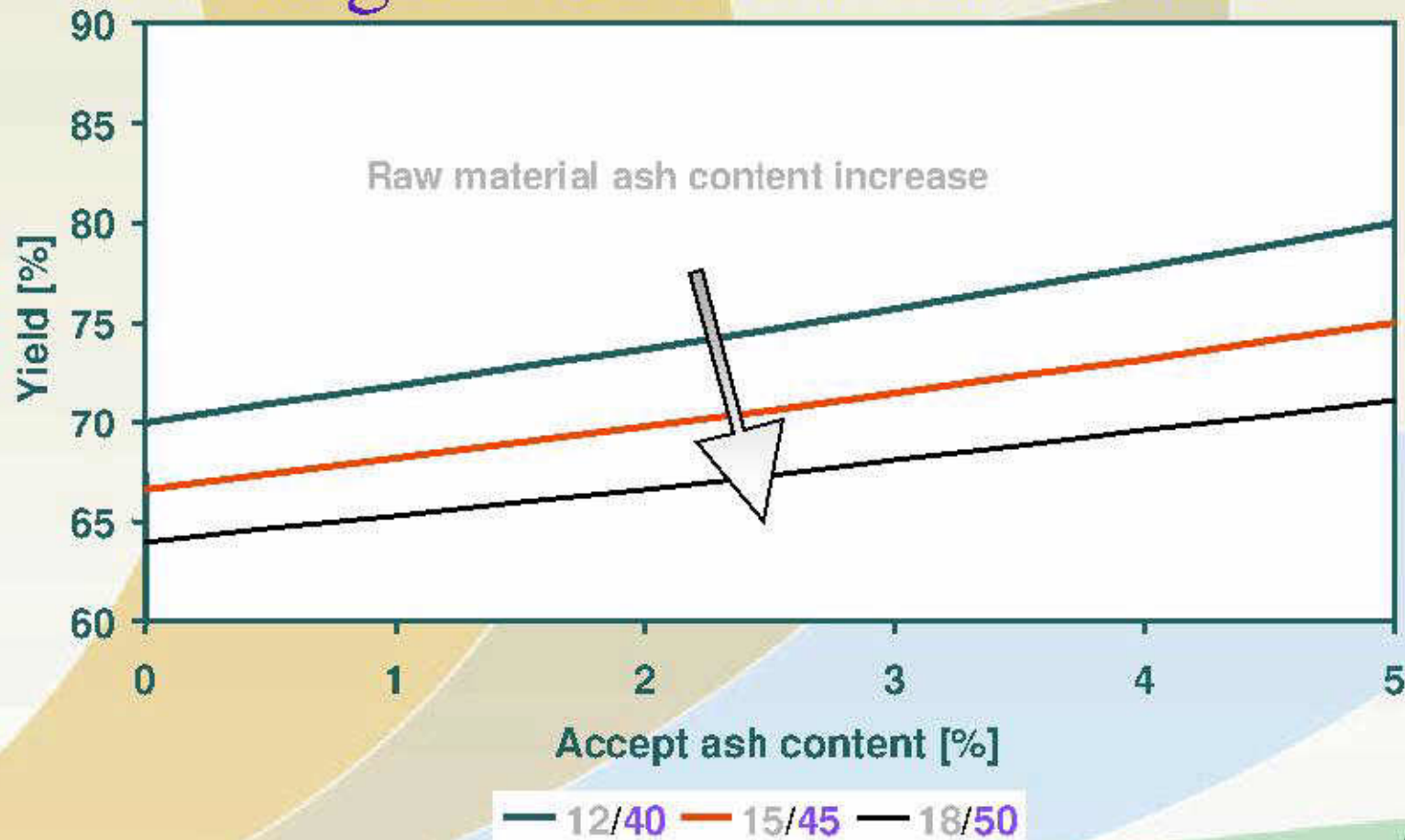
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# Yield and Ash Removal



The higher the ash removal the

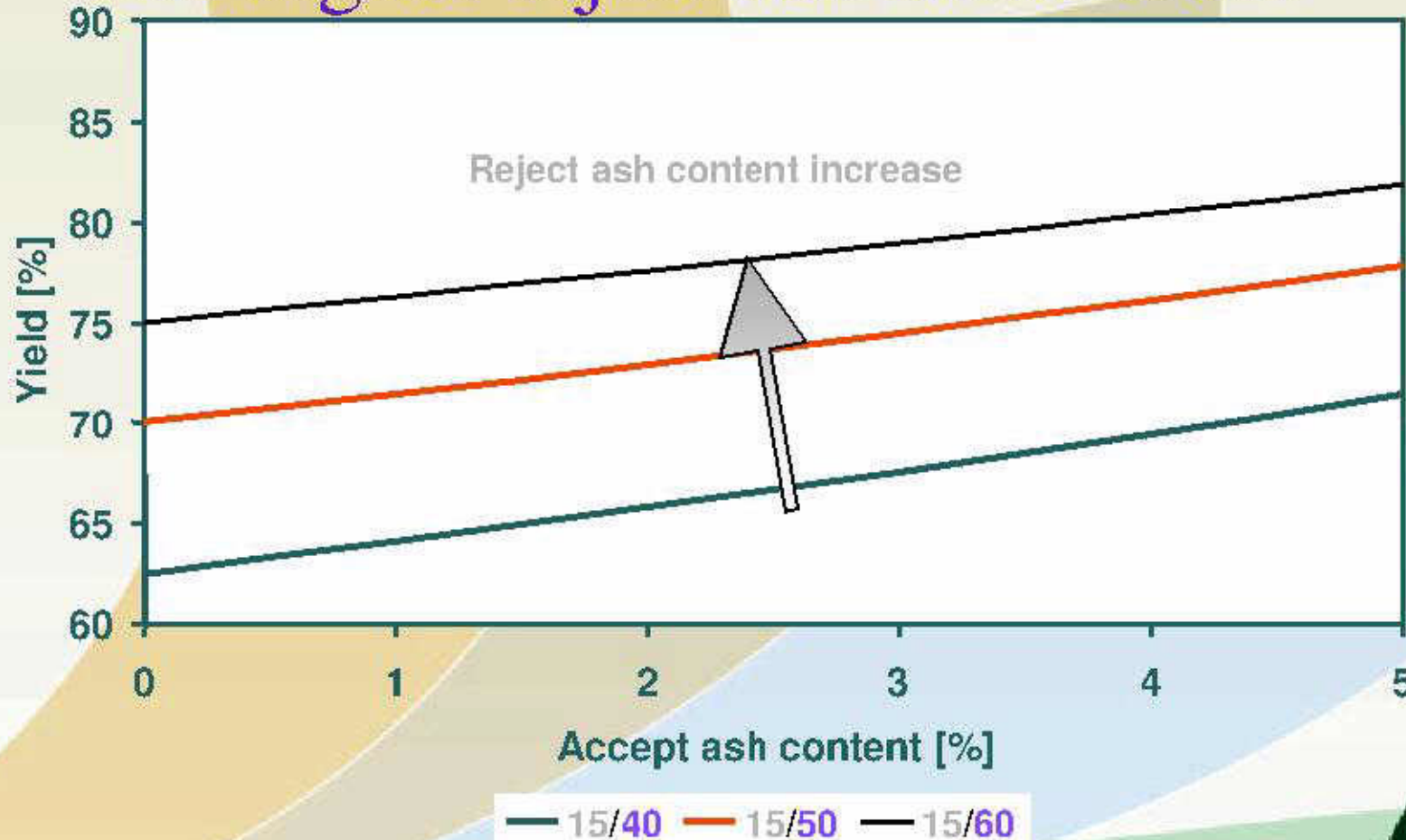


Raw material ash content (%) / Reject ash content (%)



# Yield Improvement

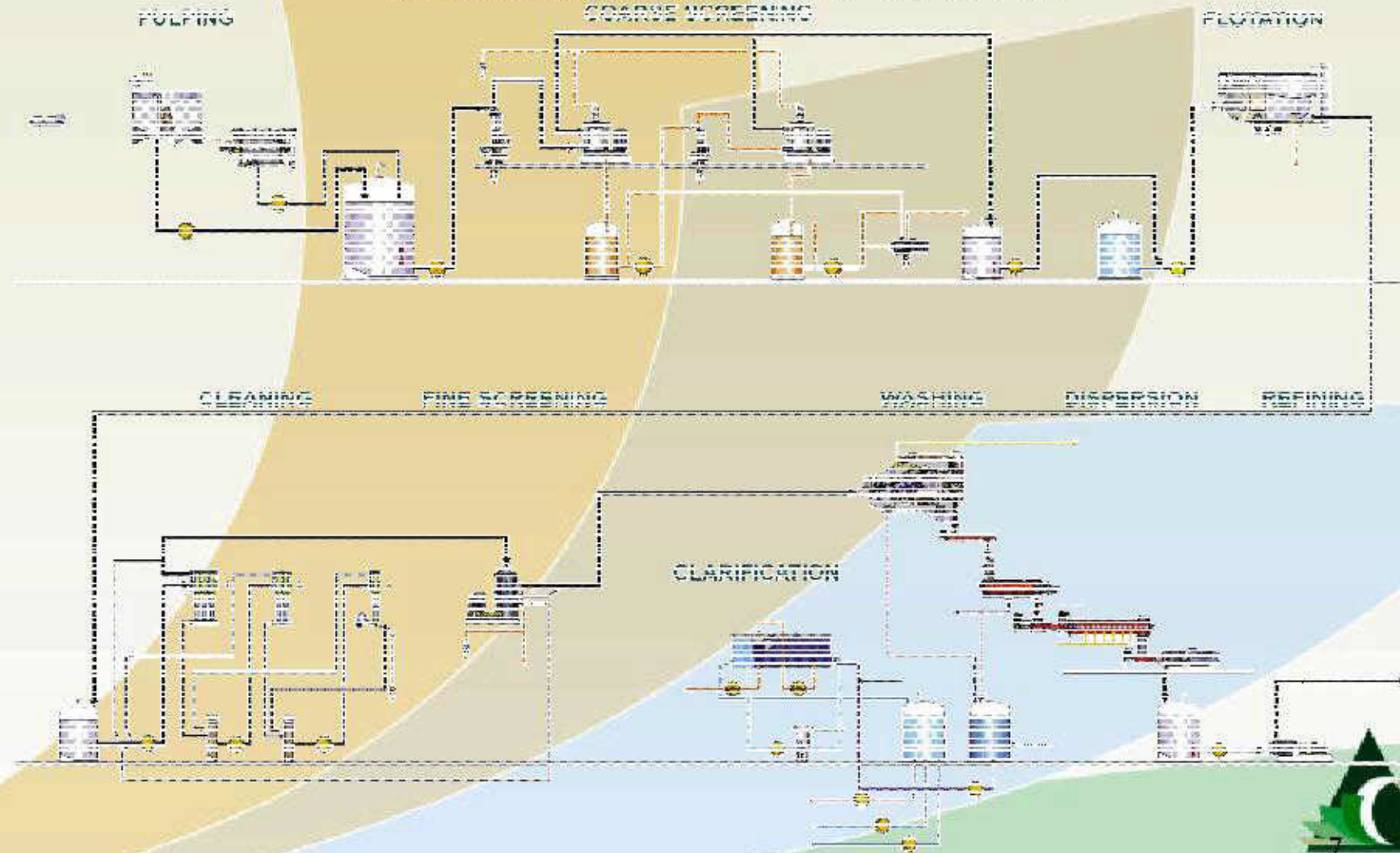
The higher reject ash content the



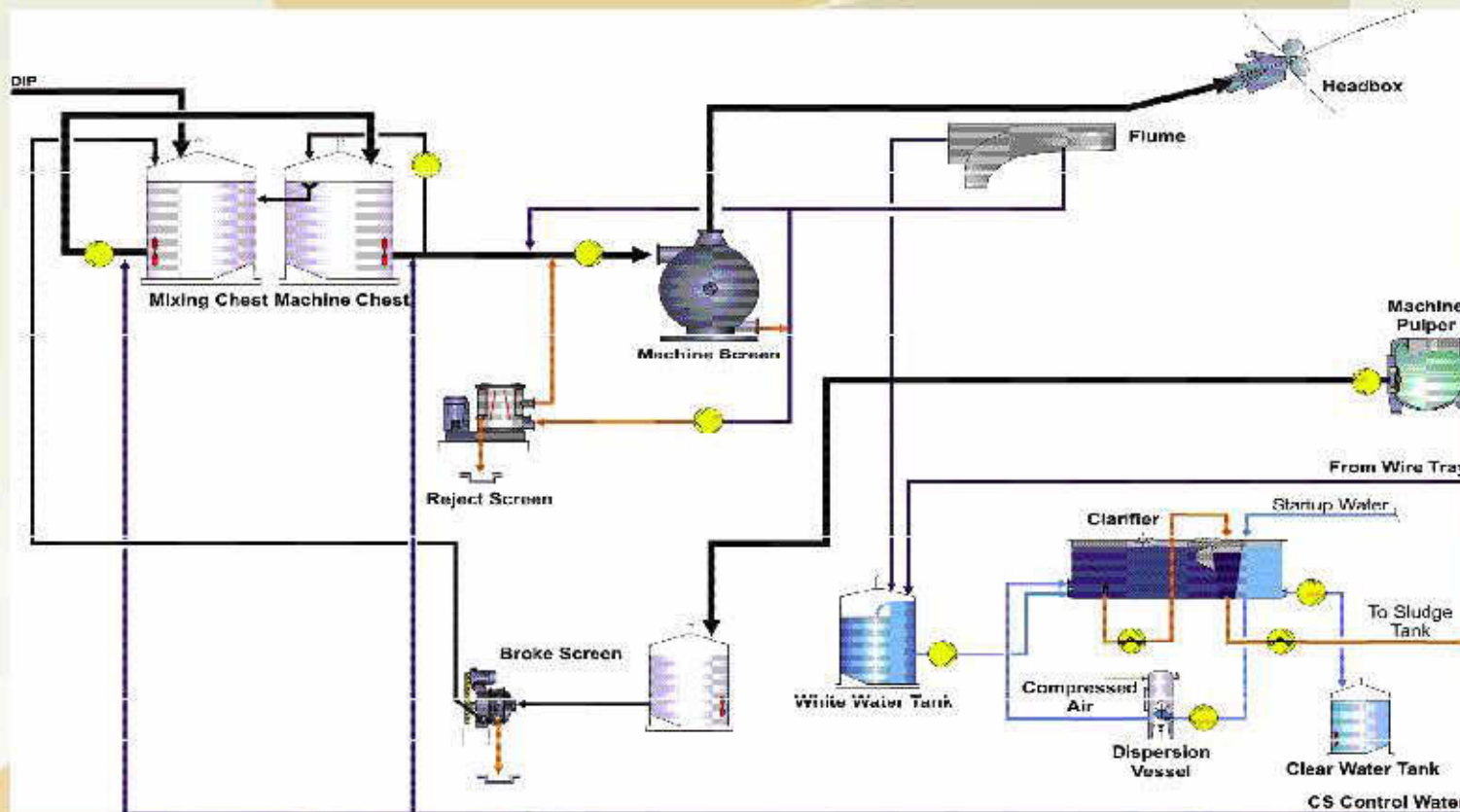
Raw material ash content (%) / Reject ash content (%)

# DIP line for towel & tissue

## Cleanliness and Ash removal



# Stock preparation flowsheet



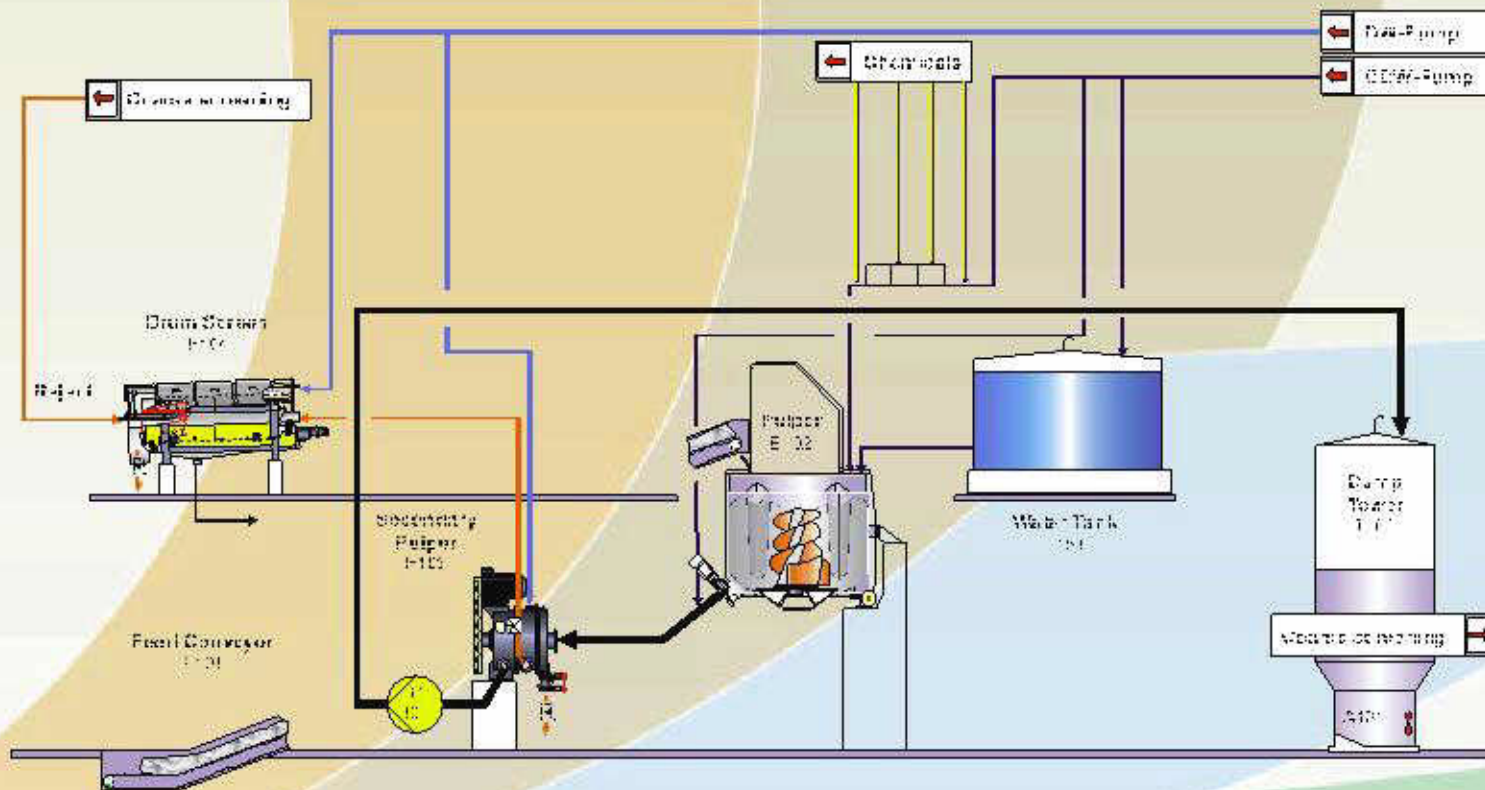


# System performance

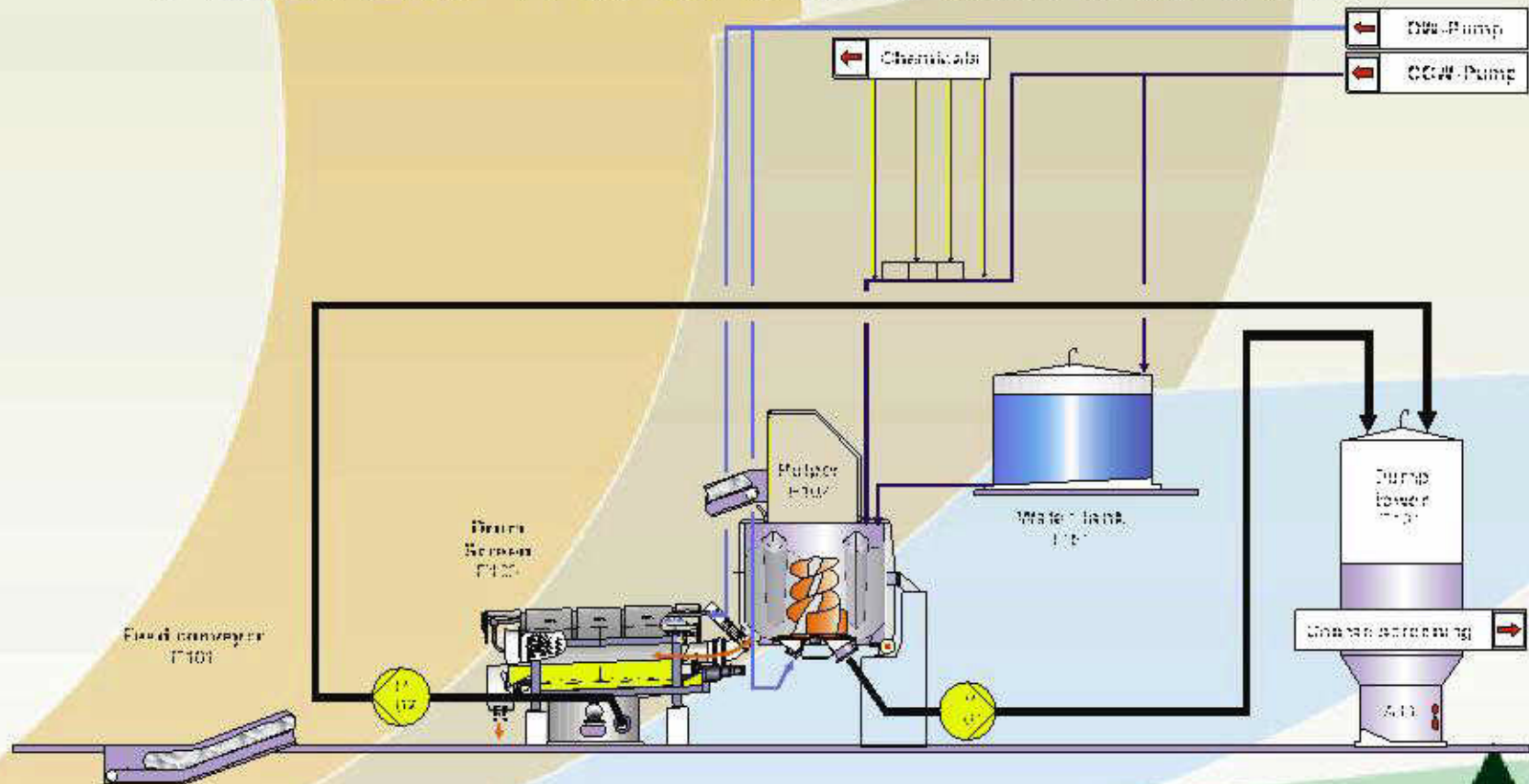
## Tissue and towel production

Target value	Performance	
	TOWEL	TISSUE
Brightness (ISO %)	55/60	72/82
Ash content (%)	3-7%	<3%
Yield (%)	70-75%	65-70%
Analysis	Performance	
	TOWEL	TISSUE
Ash content after pulper (%)	17,8	19,1
SR after pulper (ml)	35,0	25,0
Initial brightness (ISO %)	48,2	65,7
Ash content after deinking (%)	6,4	4,1
SR after deinking (ml)	51,1	28,0
Brightness after deinking (ISO %)	53,0	71,2
Final paper ash content (%)	4,8	2,7
Final paper brightness (ISO %)	55,0	73,0

# FLOWSHEET PULPER WITH SECONDARY PULPER

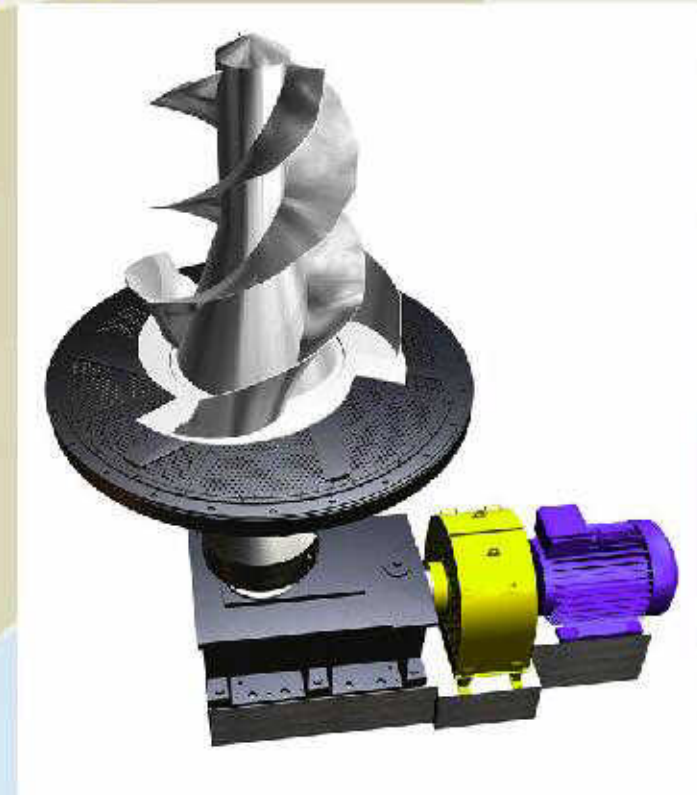
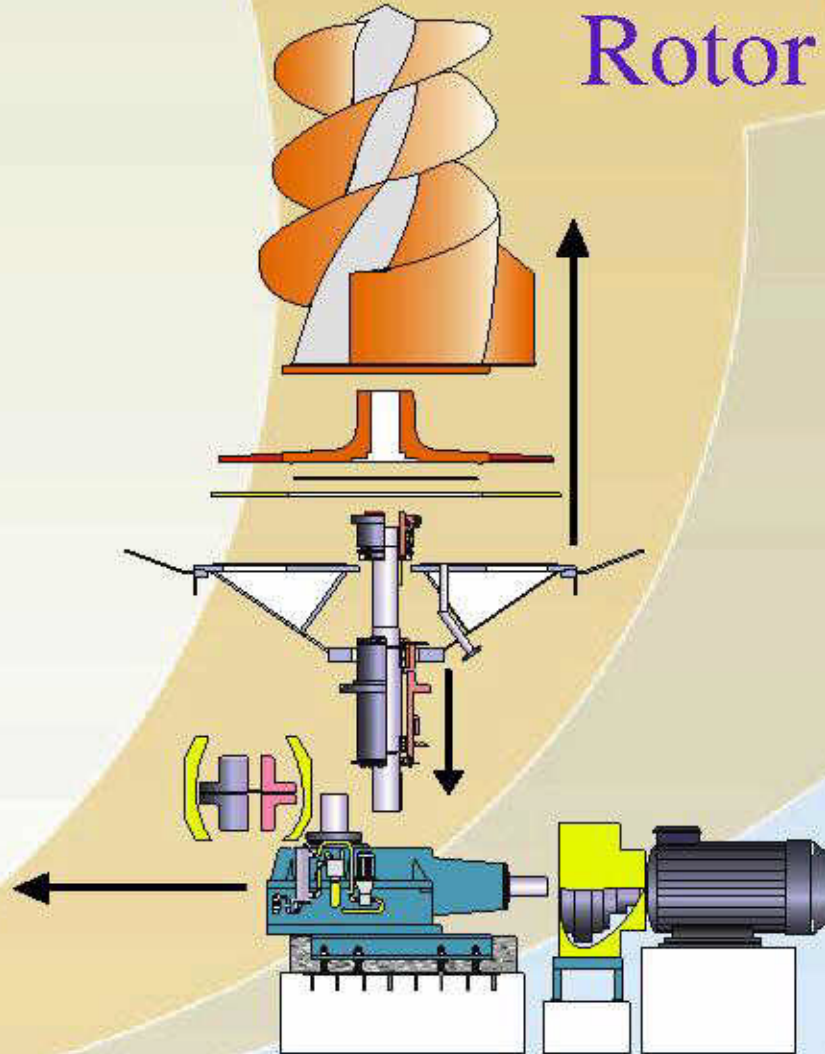


# FLWSHEET PULPER WITH SCREEN PLATE



# OptiSlush VH Pulper

## Rotor unit





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# HC BatchPulping

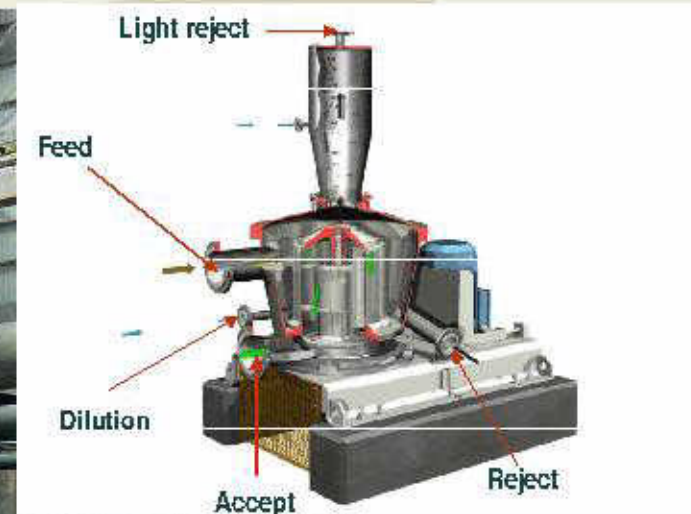


# OptiSlush VH Pulper

## Advantages

- Clean pulp for further processing
  - Efficient contaminant detachment from fibers
  - Excellent ink particle separation
- High pulp yield
  - Efficient movement of pulp
  - The special rotor design with three helical spirals ensures complete pulp movement throughout the vat.
  - Excellent defiberizing
- Efficient and Simple rejects removal
  - Helical Rotor with extraction plate and direct discharge to drum screen

# OptiScreen CS coarse screens



High capacity  
Low energy  
Low wearing



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# The purpose of DIP coarse screening

## Coarse screening tasks

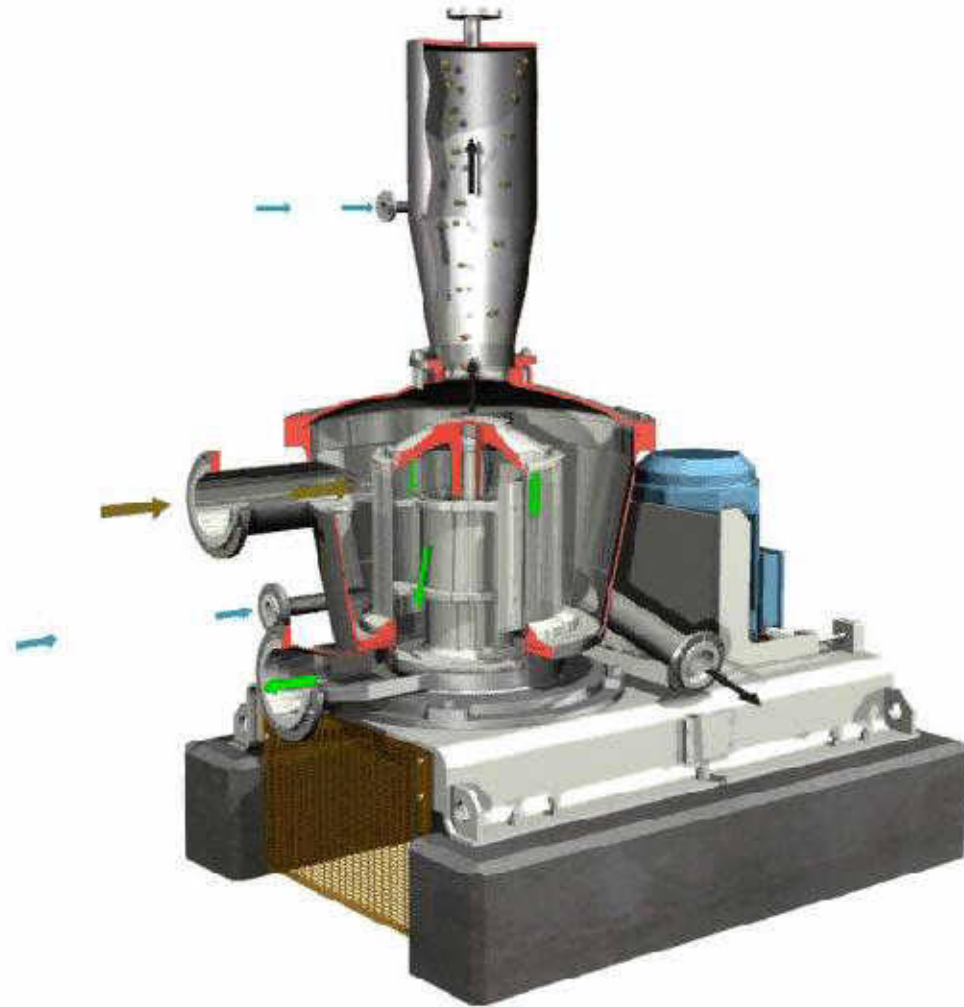
<b>Target</b>	<b>Coarse screening</b>
<b>Remove</b>	plastic, adhesives, staples, paper clips, sand, glass bigger than screen basket hole width
<b>Maximize</b>	pulp quality and constant runnability
<b>Minimize</b>	fiber loss, breakdown of impurities, energy consumption
<b>Protect</b>	pre and fine screening systems and other process stages against damages





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# Flotation



$\rho_{es}$  = Density in  
aeration sector

$\rho_{ss}$  = Density in  
separation sector

$\Delta p$  = Pressure  
difference between  
aeration and  
separation sector

High ash removal  
Low fiber losses  
Low energy  
Small layout

# Flotation

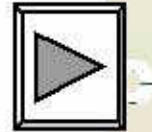
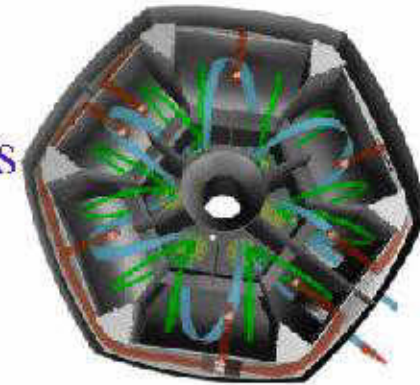
## Selective tool to remove ash

### Yield and quality depends on

- Retention time
- Feed consistency
- Control of reject overflow
  - flotation cell technology
  - foam retention time
- Ash share and fiber in reject
- Foaming
  - pulp ash content
  - chemistry
  - the amount of air
- Bubble size distribution (air feed flow vs. rotor speed, rotor type);



## Operation Principle - Basic Physics



$\rho_{as}$  = Density in  
aeration sector

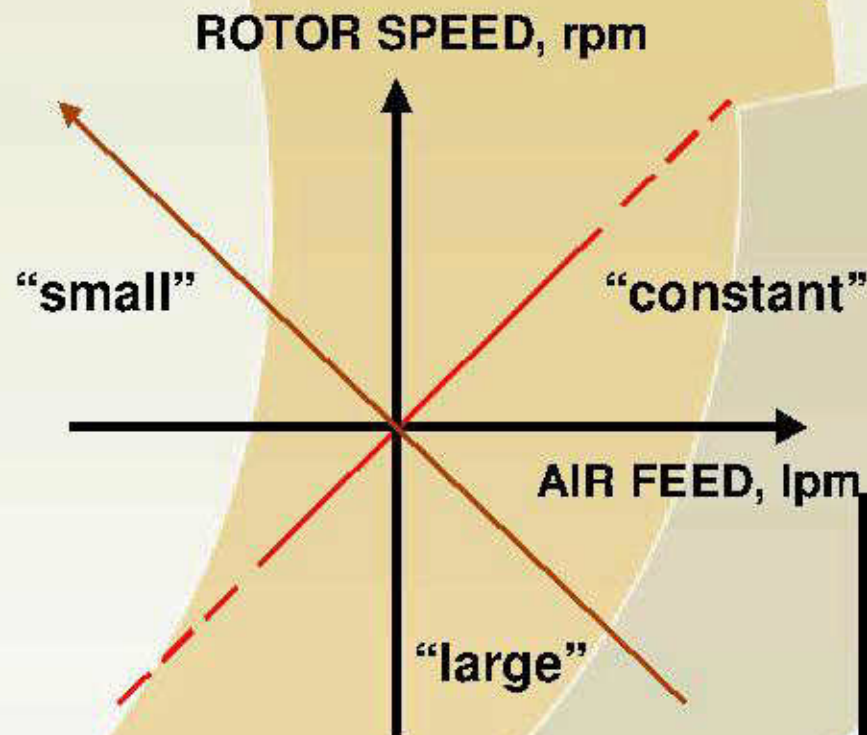
$\rho_{ss}$  = Density in  
separation sector

$\Delta p$  = Pressure  
difference between  
aeration and  
separation sector

The circulation of stock is based on the difference in the stock's specific gravity between the aeration and separation sectors.

# Flotation

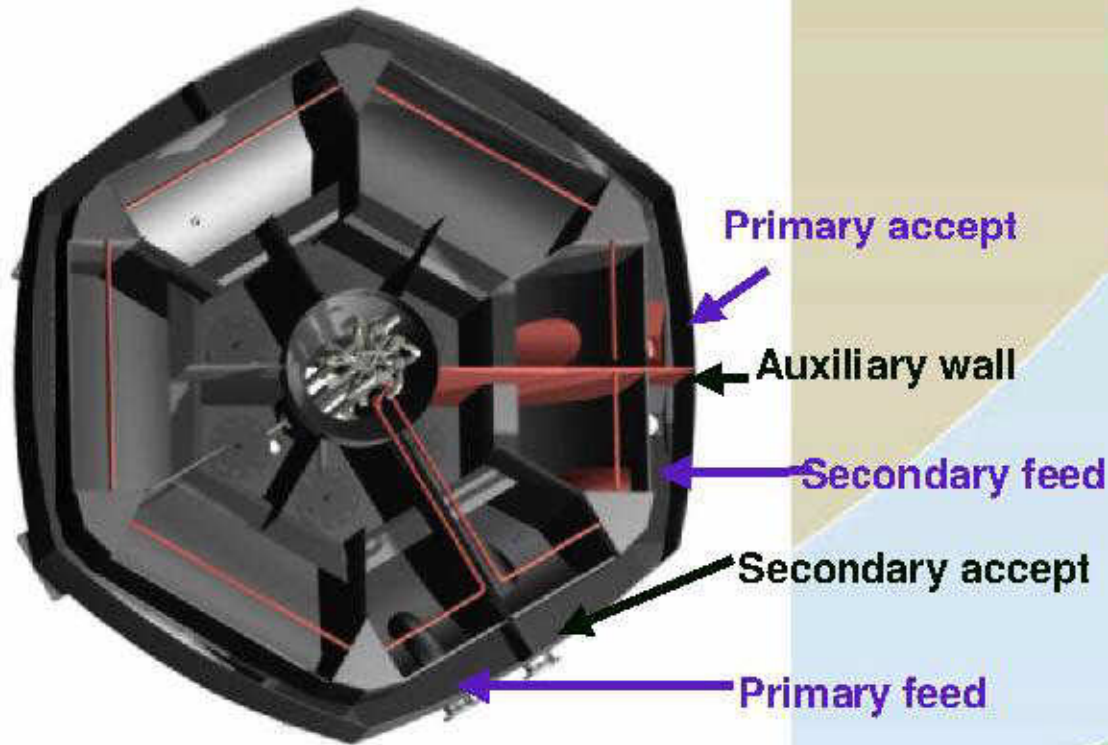
## Aeration Adjustment



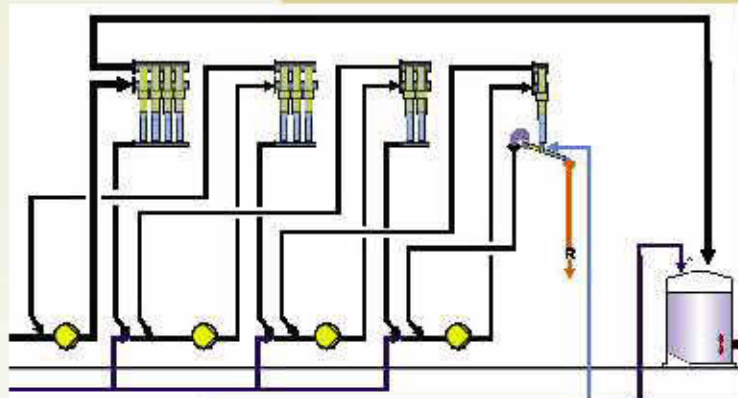
- Bubble size can be controlled by rotor speed and air feed
- Bubble size is also affected by chemistry and consistency

# OptiBright MC Flotation

## Two Stages in One Unit



# Centrifugal Cleaning



Objectives:

- Spec and Sand Removal Higher Consistencies
- Protection to the Fine Screens against wear

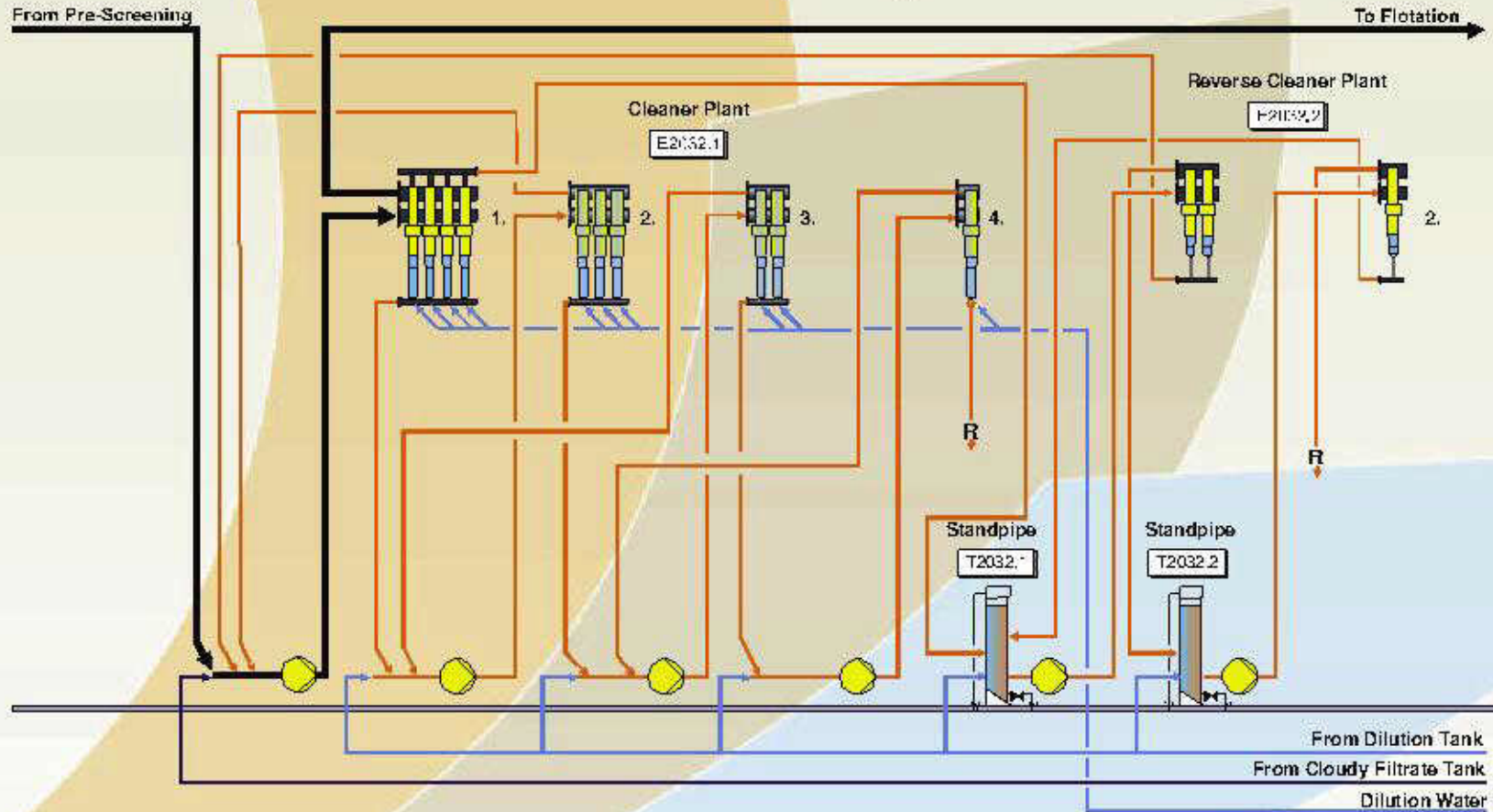


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# Cleaning



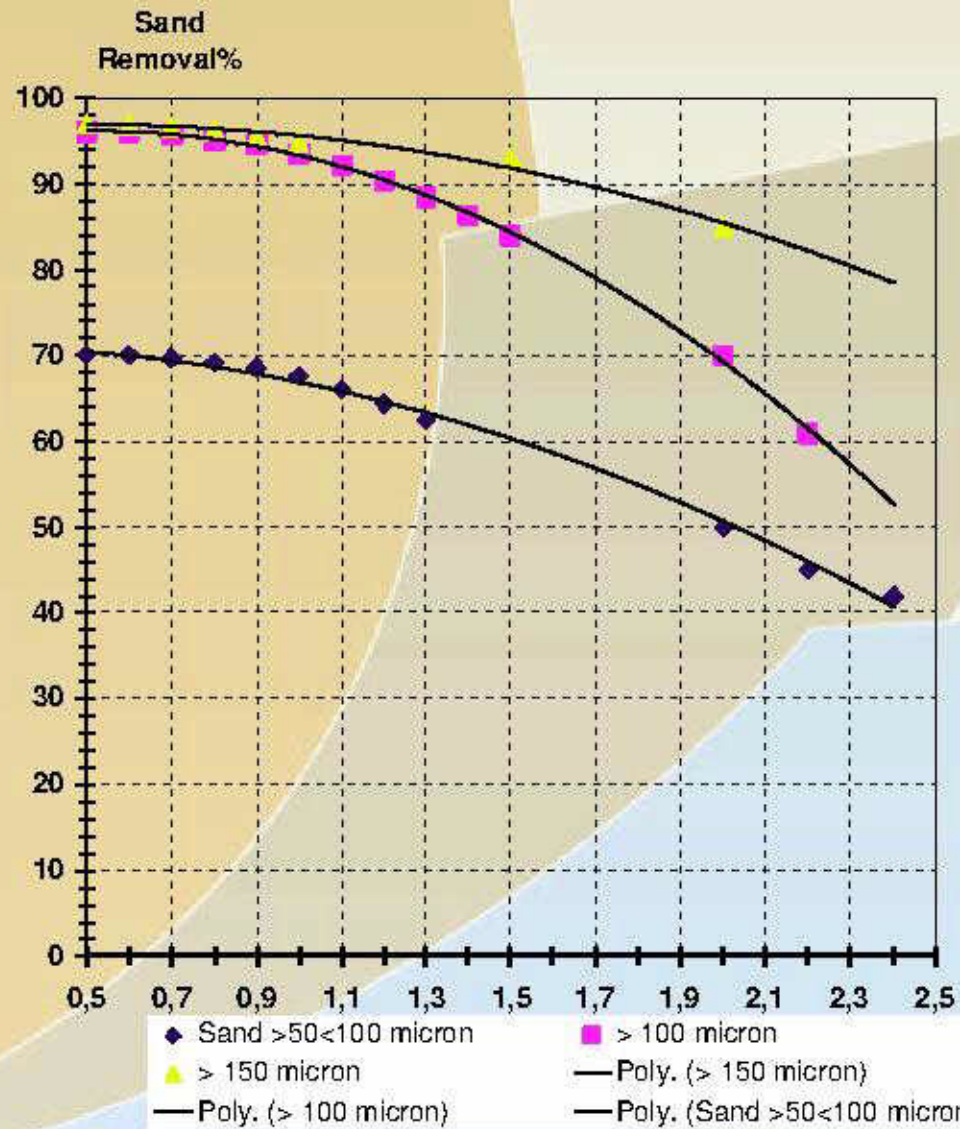




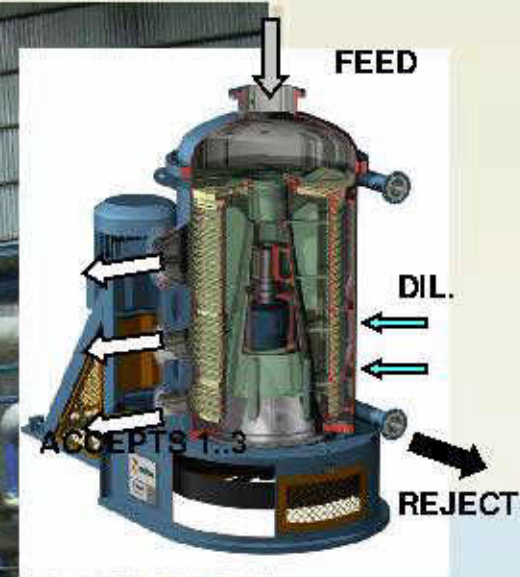
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### Clp 700 CRC at 150 kPa (21 psi) PD



# Multi-stage OptiScreen FS



Low total investment  
Low total energy  
Small layout

## Pre and fine screening

### Typical challenges in the screening systems

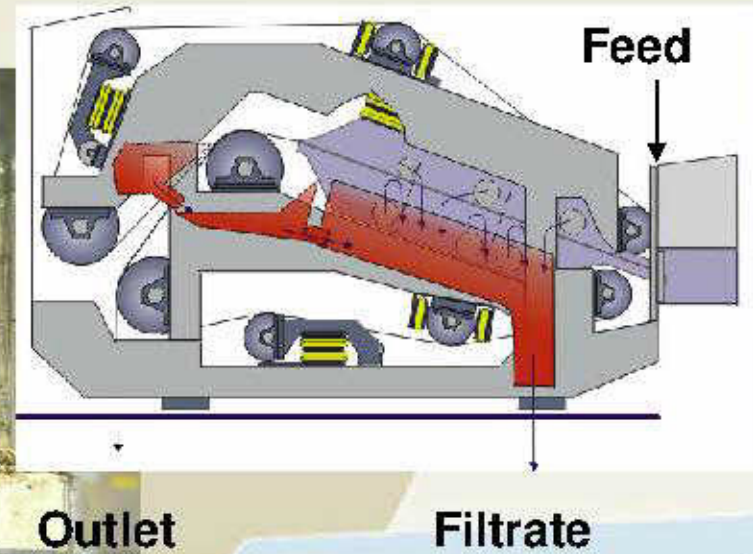
Problem	Consequence	Cost
Low separation of stickies	Lower overall sticky removal	Poor paper machine runnability
Low separation of dirt	Dirt specks on sheet	End product attractiveness and price
Low separation of heavy reject	Screen basket wear	Short screen basket life-time
High fiber loss	More raw material needed	Cost of fiber, reject treatment cost
Poor runnability	Disturbancies in production	Lost production
Frequent mechanical failures	Increased need for maintenance	Maintenance cost, lost production

# Multi-Stage Fine Screen

- Low or Medium Consistency Operation
- Low installation costs
- Eliminates intermediate tanks, pumps, controls, pipes, etc

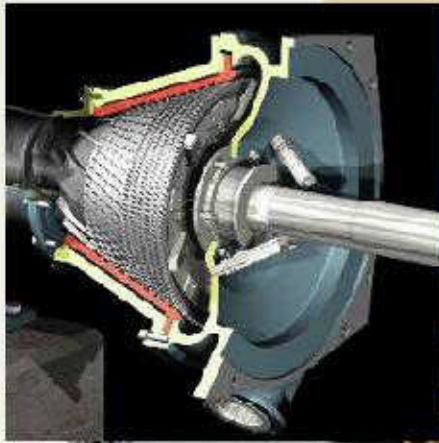


# OptiThick GapWasher



- High capacity
- Controlled washing/yield
- Low fiber losses
- Compact layout

# OptiFiner Dispersion



Efficient heating & bleaching (HI)  
Compact heating (CT)  
Strength improvement

# OptiFiner RF Refiner



Optimum refining result  
Low total energy  
Small layout

# OptiDaf Microflotation



Compact layout  
Uniform water quality



# Summary

## End product demands, raw material & operational costs

- Innovative unit process technologies
  - Efficient screening => runnability of washer and PM
  - Adjustable flotation
  - Controllable washing combined with DAF=> high ash and microsticky removal
  - Conical disperger => high dirt reduction and development of strength properties
- High production rate (even 86 tpd)
- Low water consumption (6-7 m<sup>3</sup>/t)
- Excellent process performances
  - Yield > 65%
  - Ash reduction > 80%
  - SRE > 96%
- Concept life-time cost efficiency



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# OBRIGADO

